

Secondary organic aerosol formation from small scale wood stoves

Can it be reduced by application of catalytic VOC converters?

Simone Pieber¹ – *emissions measurements*

Paul Scherrer Institute, Laboratory of Atmospheric Chemistry, Villigen
simone.pieber@psi.ch, 0041 056 310 4467

Anastasios Kampolis² – *catalyst development*

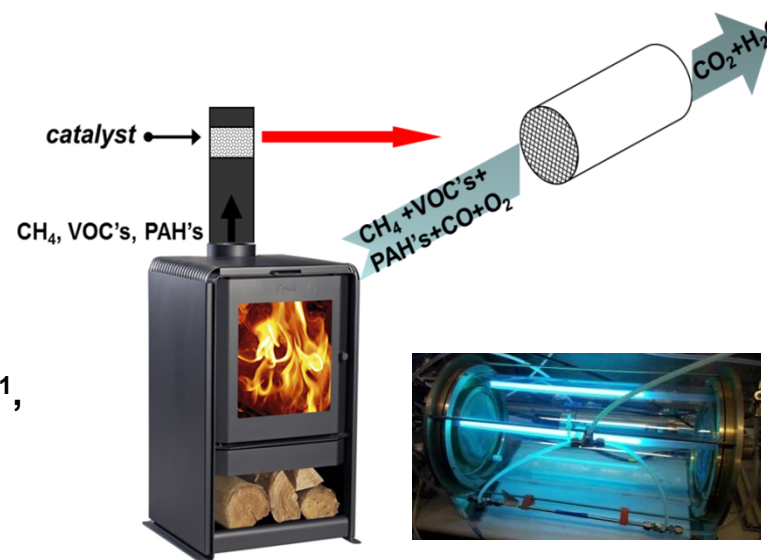
Paul Scherrer Institute, Bioenergy and Catalysis Laboratory, Villigen
anastasios.kampolis@psi.ch, 0041 056 310 5321

**Emily Bruns¹, Imad El Haddad¹, Dogushan Kilic¹,
Davide Ferri², Oliver Kröcher^{2,3},
Urs Baltensperger¹ and André S.H. Prévôt¹**

¹ Laboratory of Atmospheric Chemistry, Paul Scherrer Institute

² Bioenergy and Catalysis Laboratory, Paul Scherrer Institute

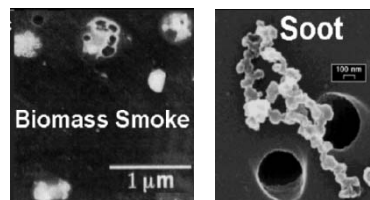
³ École Polytechnique Fédérale de Lausanne



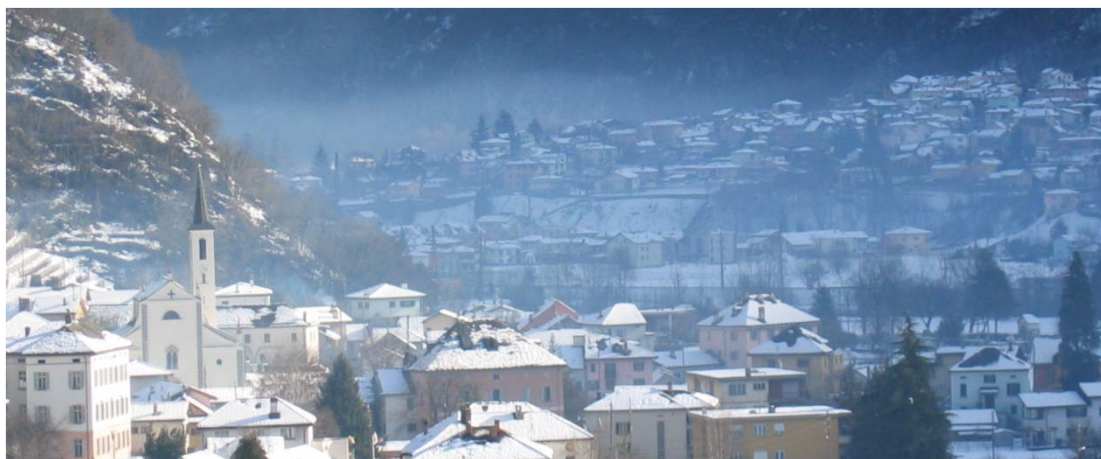
INTRODUCTION

Residential log wood combustion

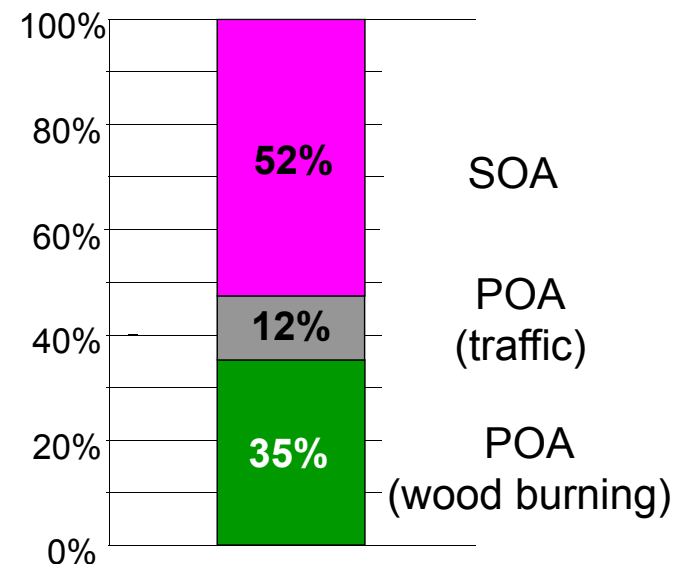
- common heating method
- black carbon, primary organic aerosol (POA)
- gasphase hydrocarbons
- significant formation of secondary organic aerosol (SOA)



(Heintzenberg et al., 2003)



Organic Particulate Mass



Average organic components in Winter from various sites in central Europe

(Lanz et al., ACP., 2010)

GASPHASE EMISSIONS

average exhaust composition

CO₂ up to 10.000 ppm

CO up to 5000 ppm

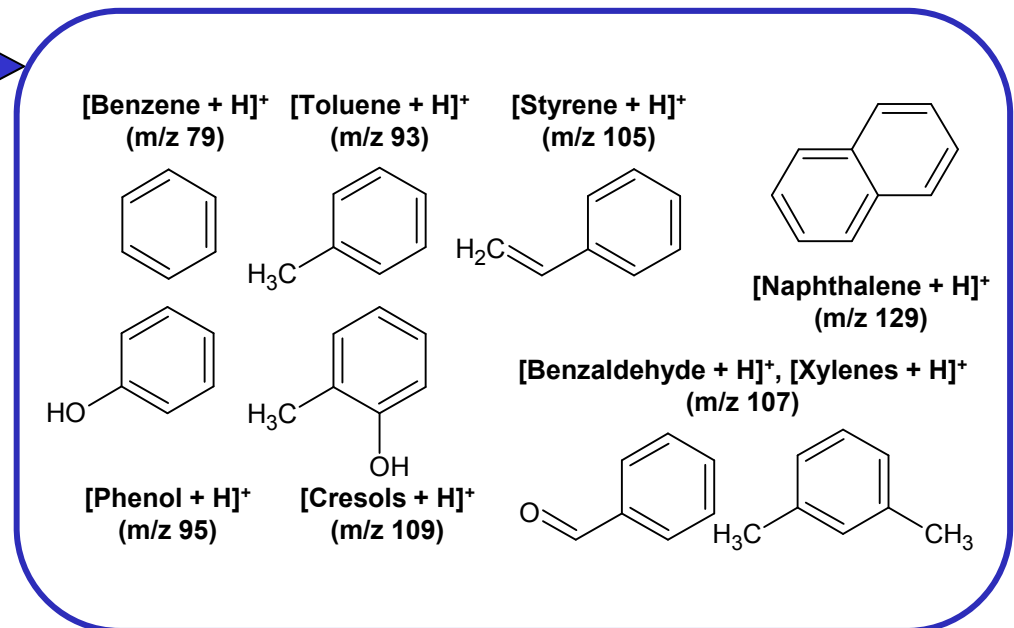
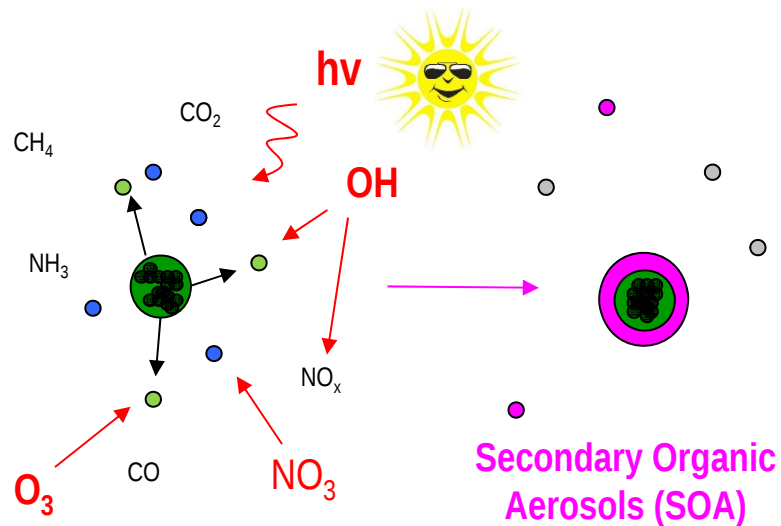
CH₄ up to 500 ppm

H₂O up to 8 vol.%

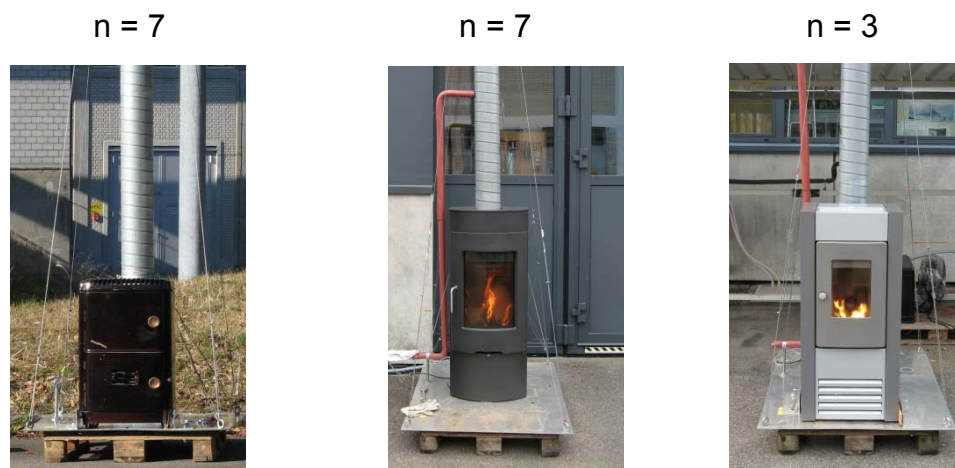
NMHC up to 1000 ppmC

NMHC fraction can be dominated by (polycyclic) aromatic hydrocarbons

⇒ deleterious health effects
⇒ increased formation of secondary organic aerosol in atmospheric aging

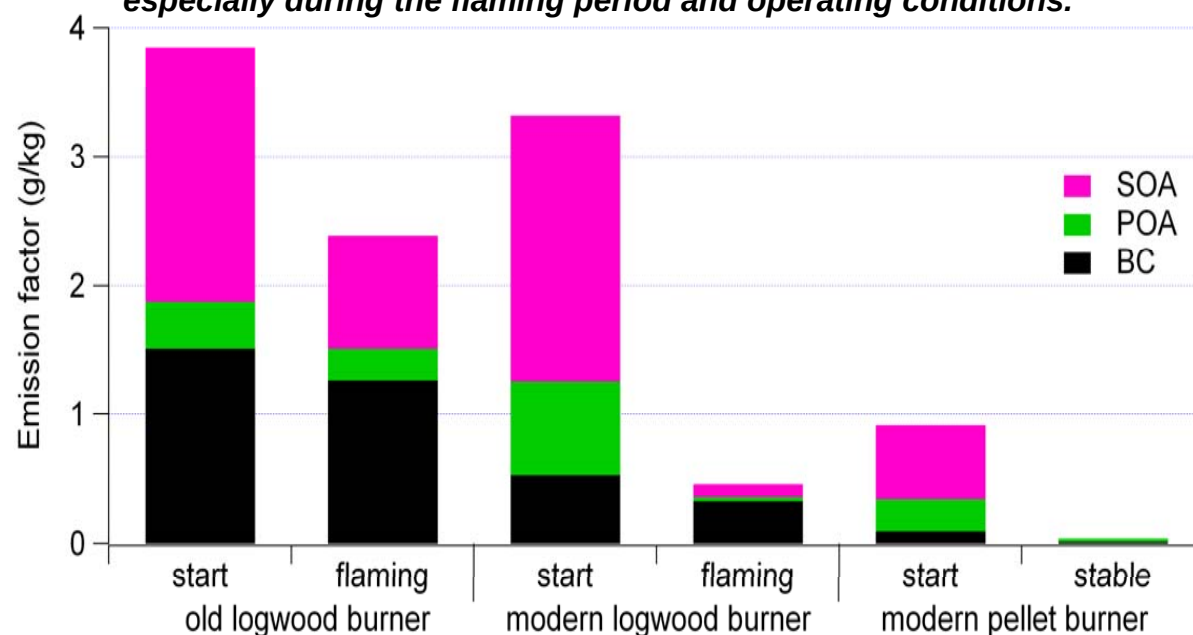


SECONDARY ORGANIC AEROSOL



POA and BC can be reduced by optimization of the oven design, especially during the flaming period and operating conditions.

After-treatment options:



needs (catalytic) reduction of precursors (NMHC)
could be reduced with mechanical methods

PROJECT IDEA

Bioenergy and Catalysis
Laboratory, PSI0

➤ Efficient catalyst for oxidation of CH_4 and NMHC at low temperature

➤ Pt / Al_2O_3 and Pt / x% CeO_2 - Al_2O_3

- powder (model gas, H_2O stability)
- coated monolith
 - ✓ model gas vs. real wood burning exhaust
 - ✓ effect on NMHC & secondary organic aerosol

Al_2O_3

- great mechanical properties
- high surface area - porosity
- water resistant

Pt

- high activity for CO and HC
- fair stability against poisoning
- H_2PtCl_6 left overs may prevent poisoning by inorganic compounds

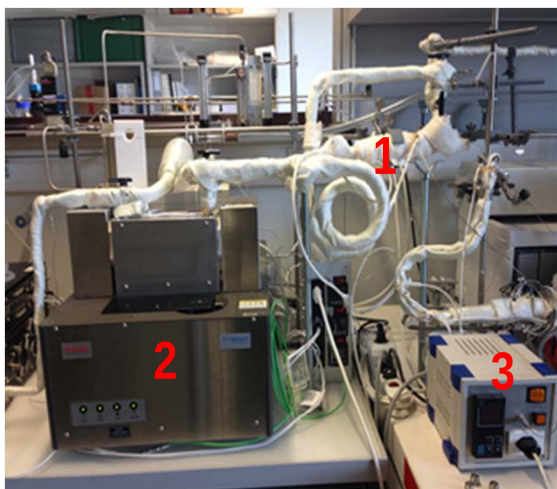
CeO_2

- high oxygen storage capacity (OSC)
- improves dispersion of supported metal:
*smaller metal clusters,
more active centers in metal-support interface*
- enhances catalyst's thermal stability

EXPERIMENTAL SET-UP

Catalyst in powder form

Bioenergy and Catalysis
Laboratory, PSI



(1) Reactor, (2) FT-IR, (3) Temp. controller

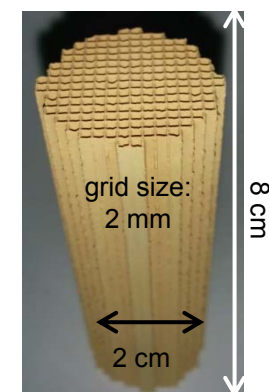
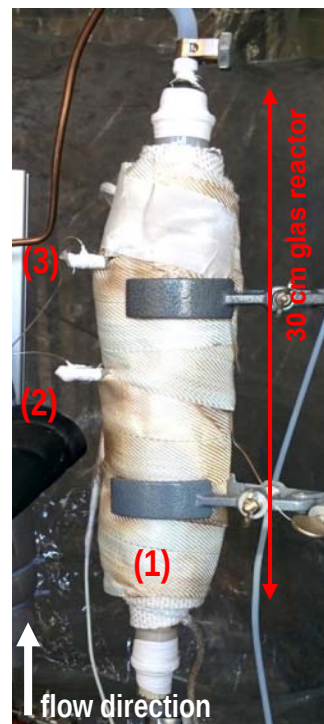
fixed-bed reactor

reaction feed: 20% O₂, 1000 ppm CH₄, balance N₂,
F = 100 mL min⁻¹, GHSV = 118 L g⁻¹ h⁻¹

(Kampolis et al., in prep.)

Catalyst coated on monolith

Bioenergy and Catalysis
Laboratory, PSI



(1) temperature controlled glass
reactor, filled with coated monolith,
(2) temp. sensor inlet,
(3) temp. sensor outlet

coating on ceramic monolith

reaction feed:

Lab: 10% O₂, 1000 ppm CH₄,
4.7% H₂O, balance N₂,
F = 8 L min⁻¹, GHSV = 180 L g⁻¹ h⁻¹

Wood Burning Exhaust, F = 6 L min⁻¹

EXPERIMENTAL SET-UP

Catalyst coated on monolith – tested with wood burning emissions

Laboratory of
Atmospheric Chemistry, PSI

Proton transfer reaction mass spectrometer (HR-PTR-ToF-MS)

Volatile organic compounds,
degree of aging (OH exposure)

Flame Ionisation Detector

CH₄, NMHC, THC

Cavity Ring Down Spectrometer

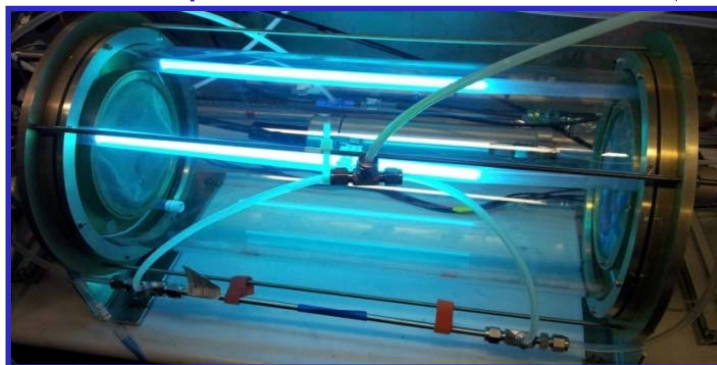
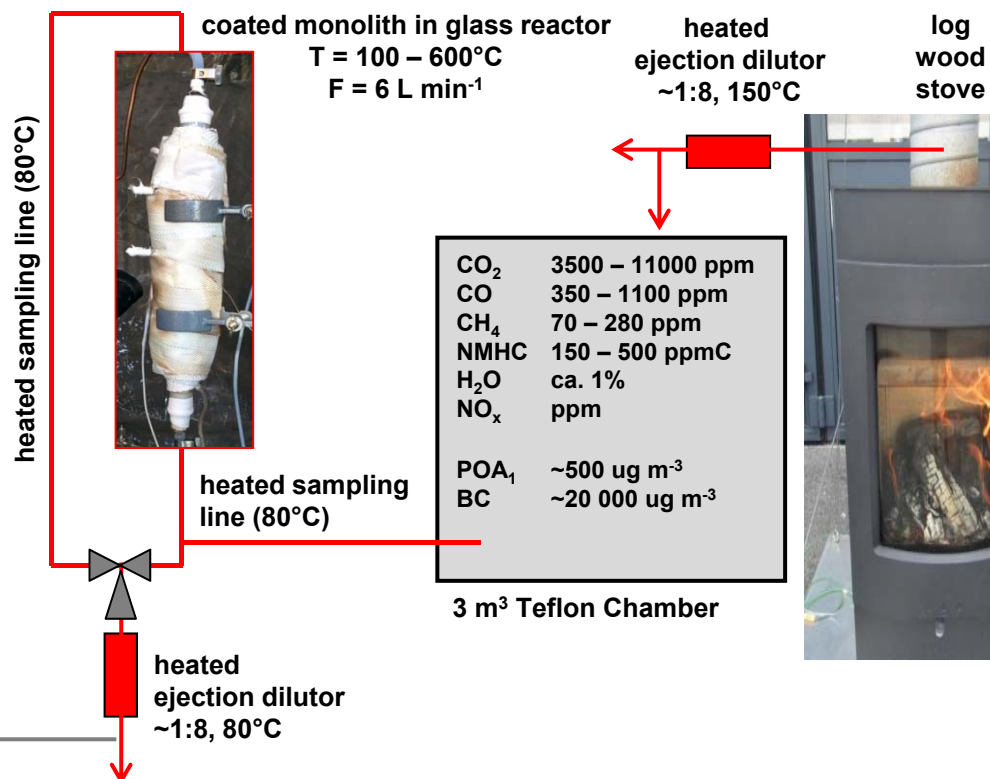
CO₂, CO, CH₄, H₂O

Aerosol mass spectrometer (HR-ToF-AMS)

Non-refractory PM quantification,
chemical composition,

Aethalometers

Black carbon (soot) quantification

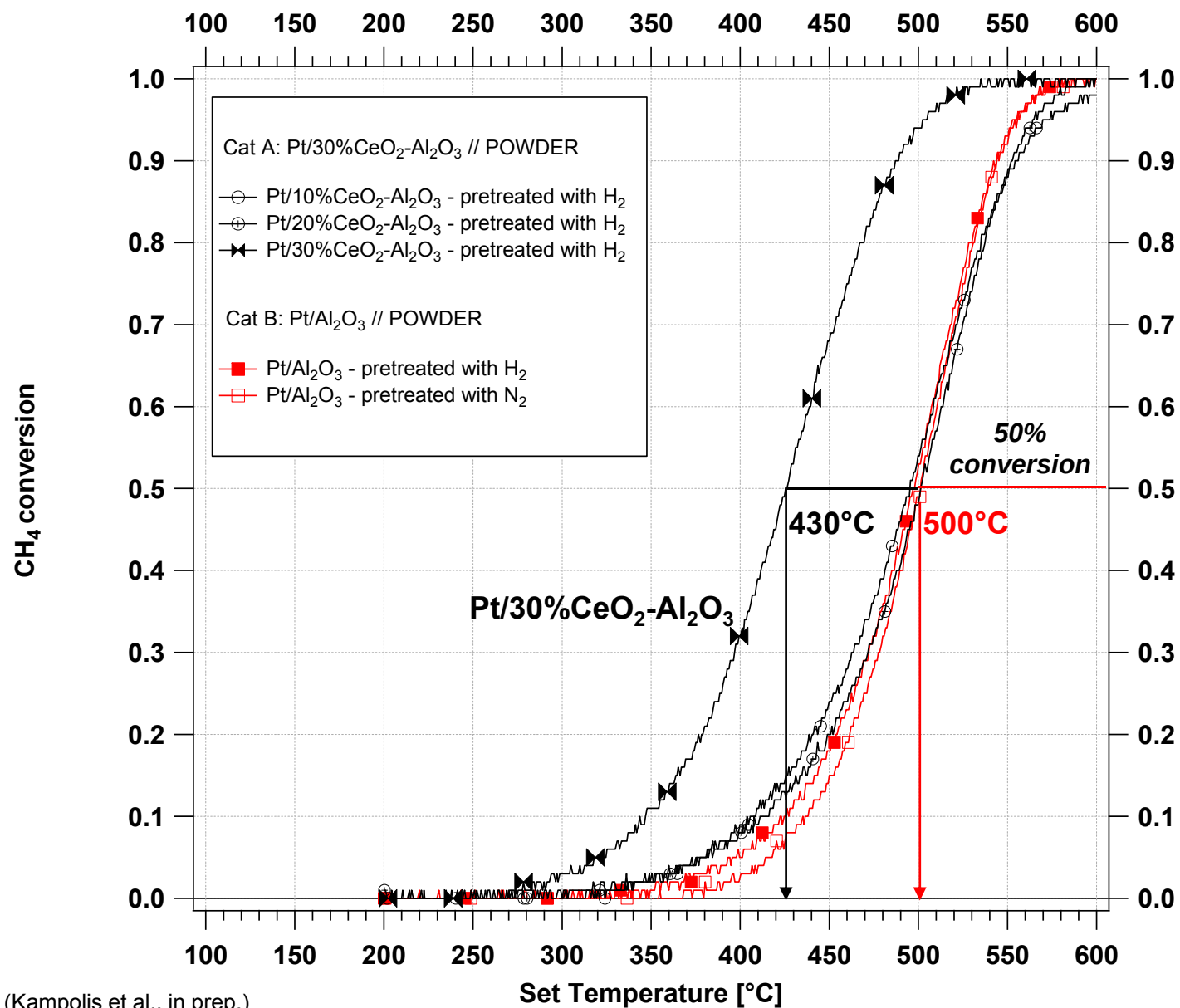


Potential Aerosol Mass (PAM) Chamber to simulate secondary organic aerosol formation

(Kang et al., ACP, 2007 and Lambe et al, AMT, 2010)

RESULTS

CH_4 conversion with powder in lab reactor

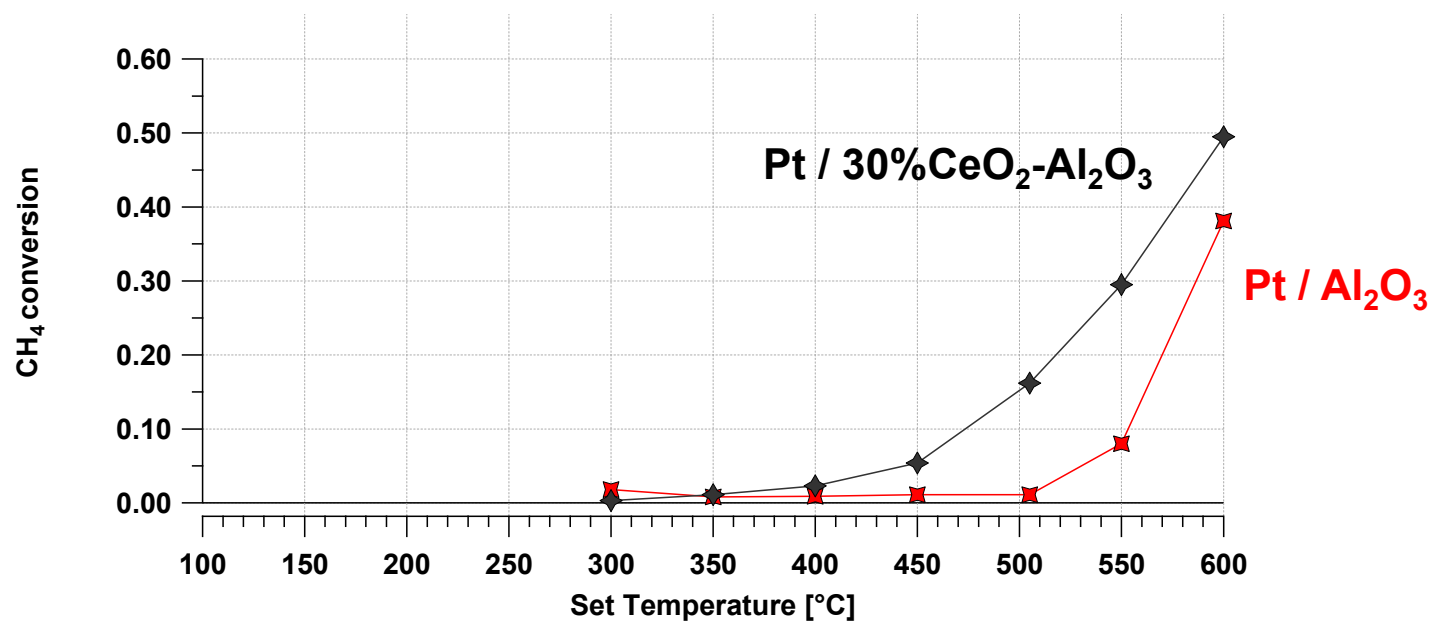
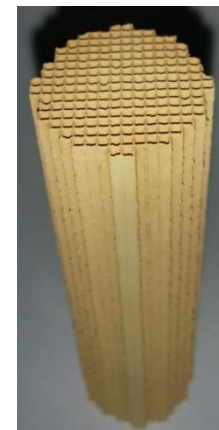


(Kampolis et al., in prep.)

CH_4 conversion with coated monoliths in lab reactor

Bioenergy and Catalysis
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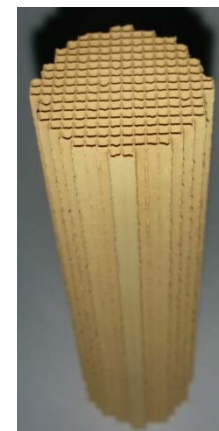
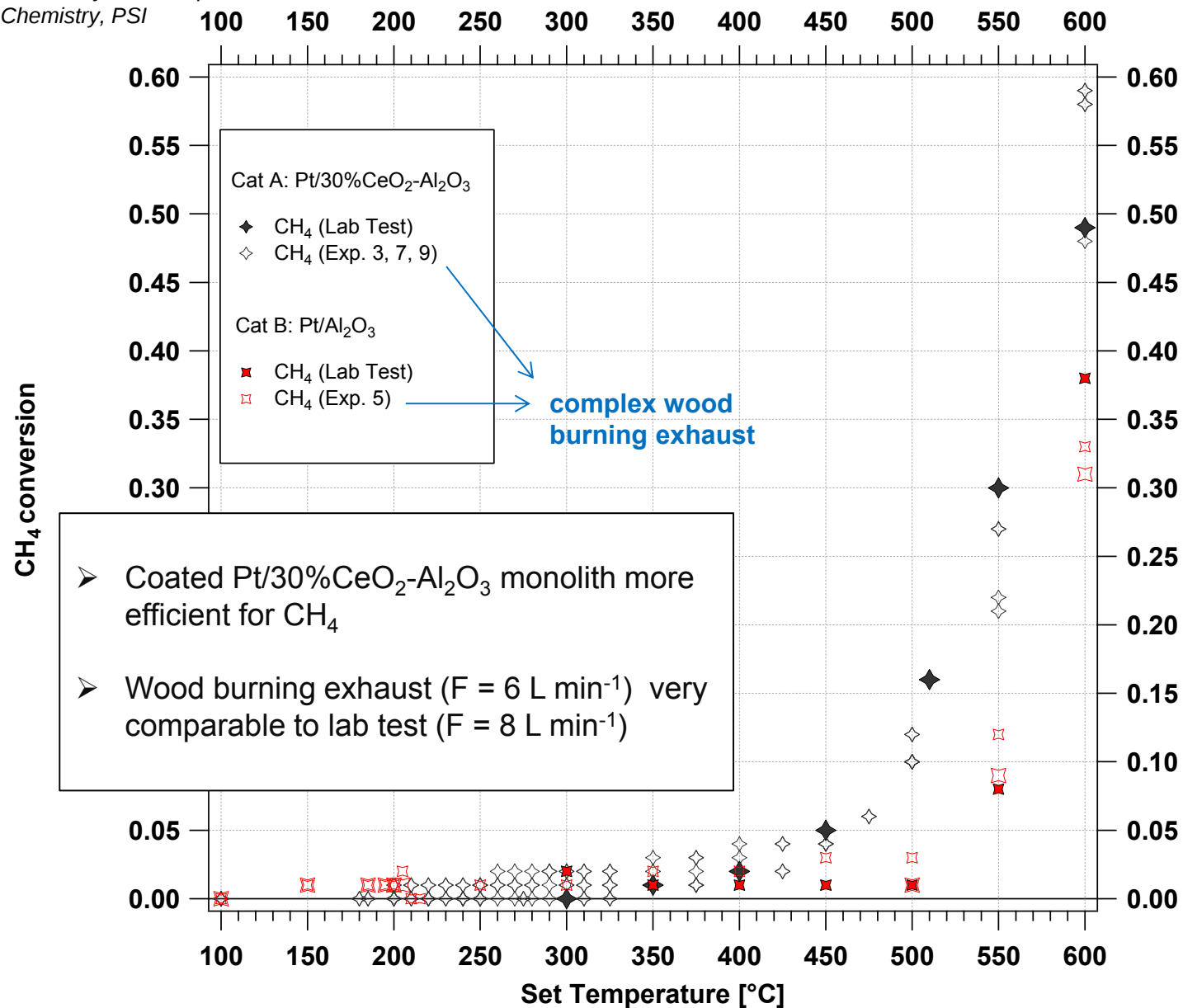
- Coated $\text{Pt}/30\%\text{CeO}_2\text{-Al}_2\text{O}_3$ monolith more efficient for CH_4
- T for 50% CH_4 conv. for monolith is 600°C vs. 430°C for powder



(Kampolis et al., in prep.)

CH_4 conversion with monolith: lab test vs. WB exhaust

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fresh

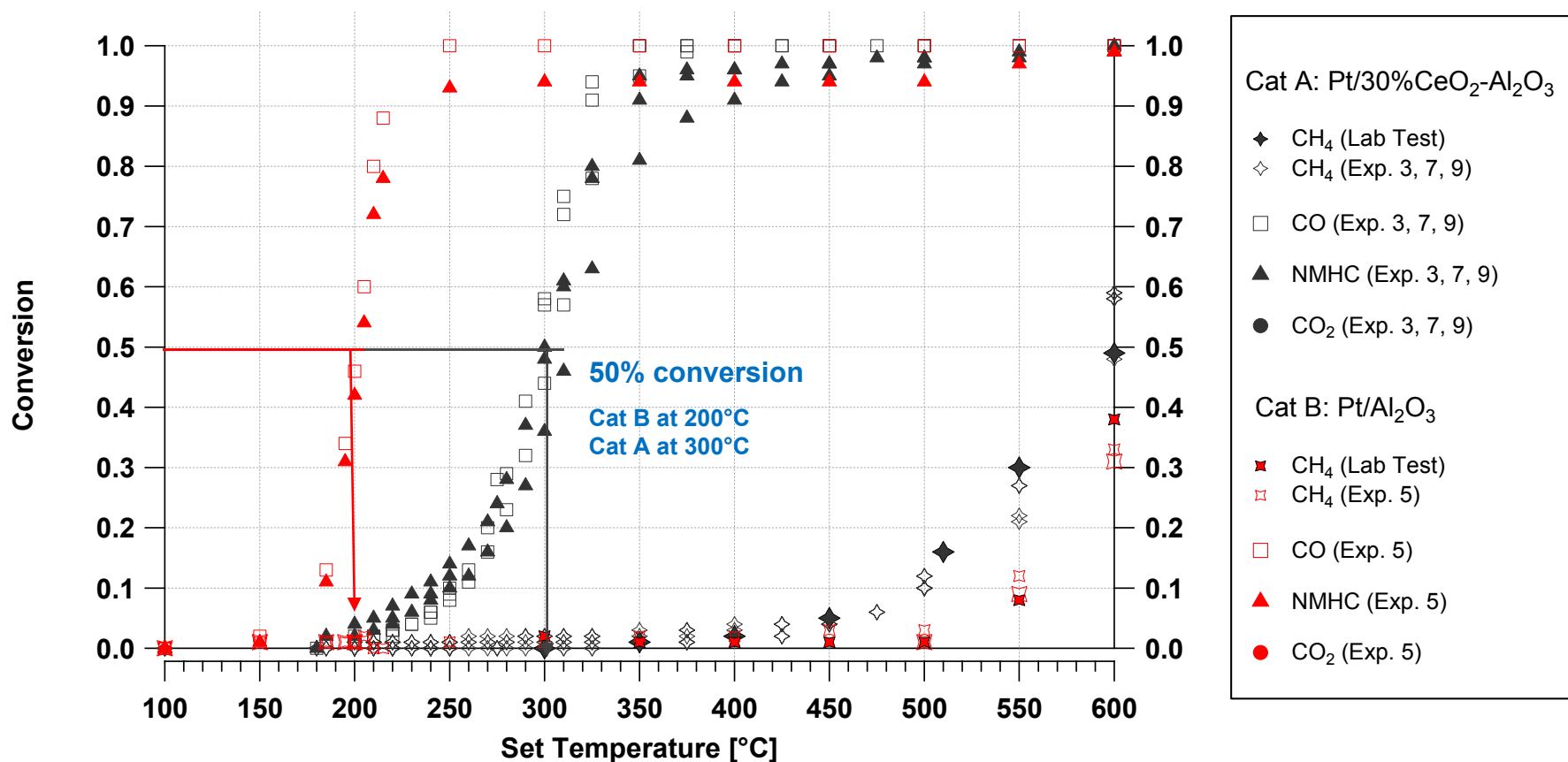
after exposure to WB



CO and NMHC conversion with monolith: WB exhaust

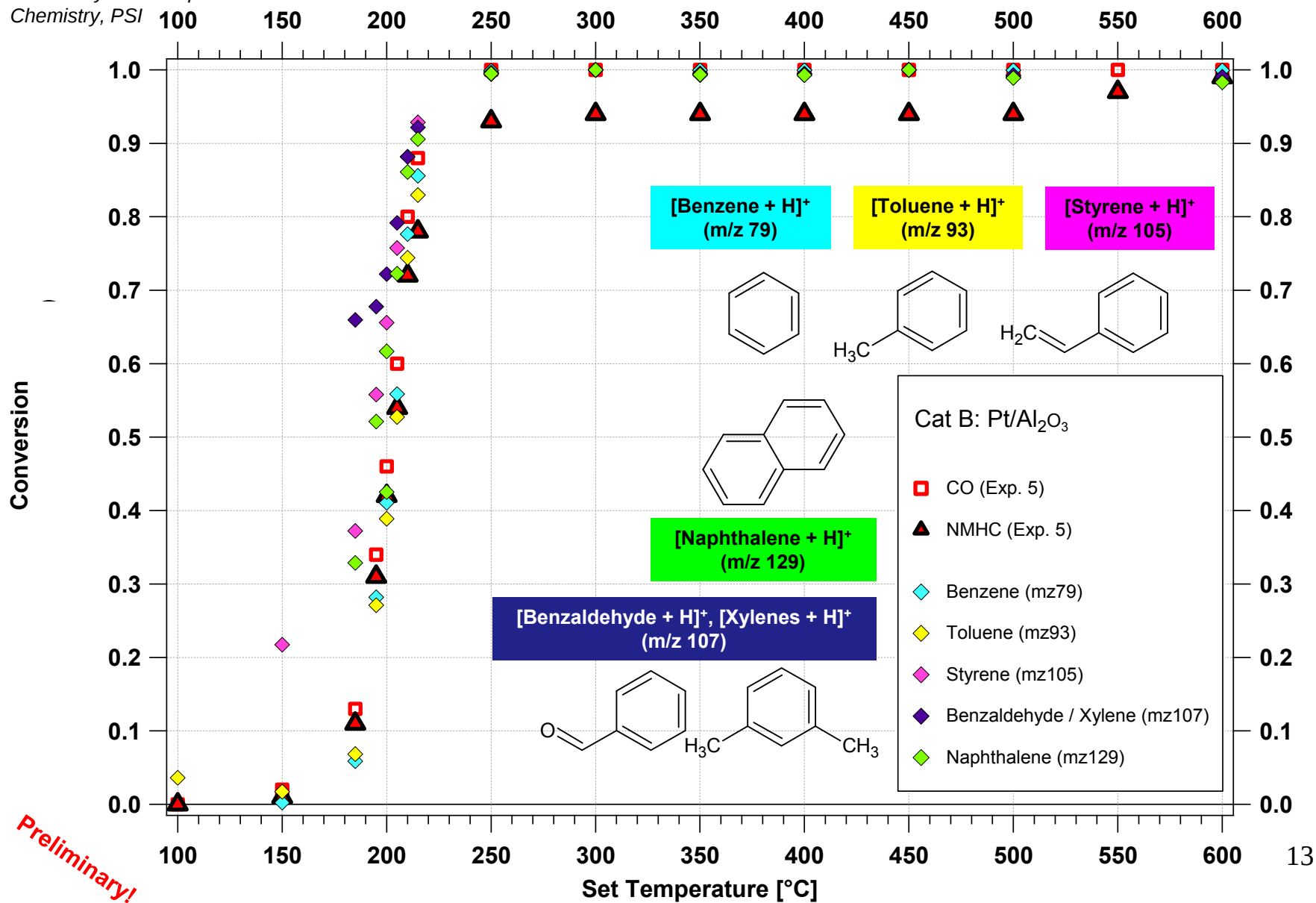
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- for CO and NMHC lower T than for CH₄
- CO and NMHC conv. with 30%CeO₂ needs further investigation



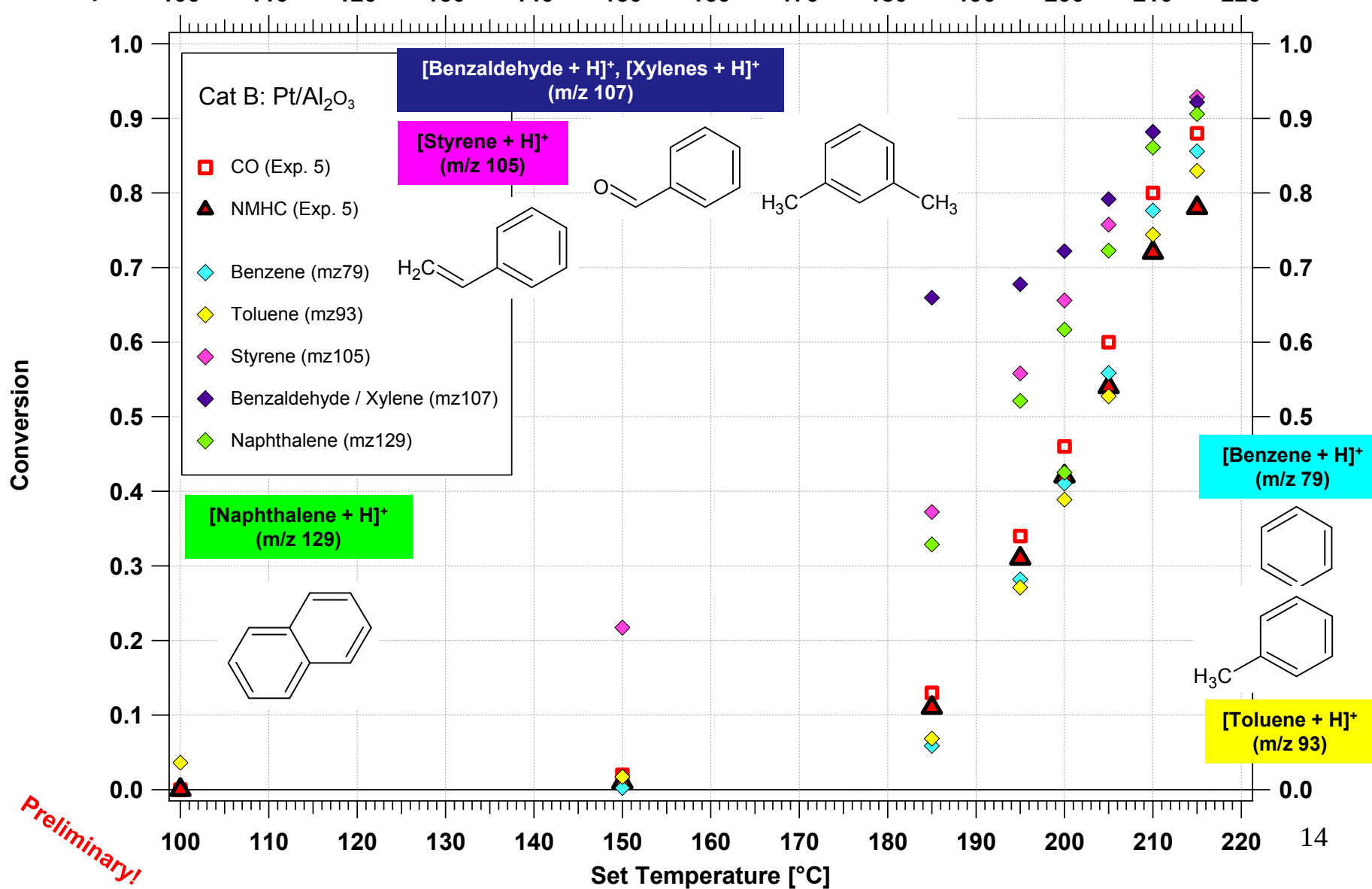
Aromatic HC conversion with monolith: WB exhaust

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Aromatic HC conversion with monolith: WB exhaust

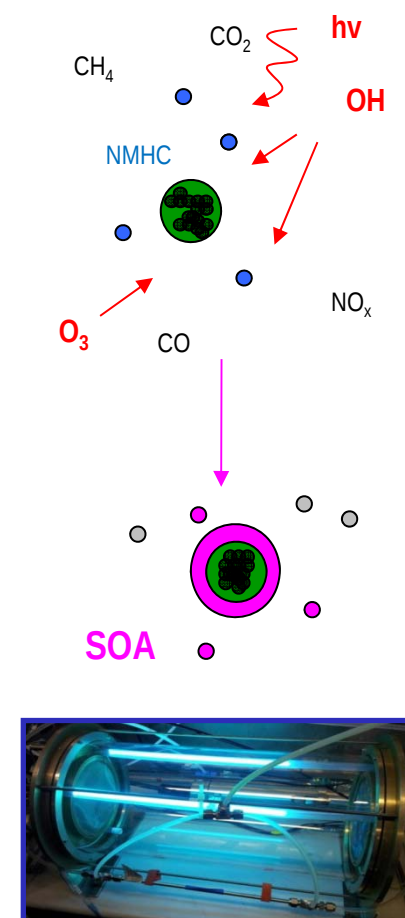
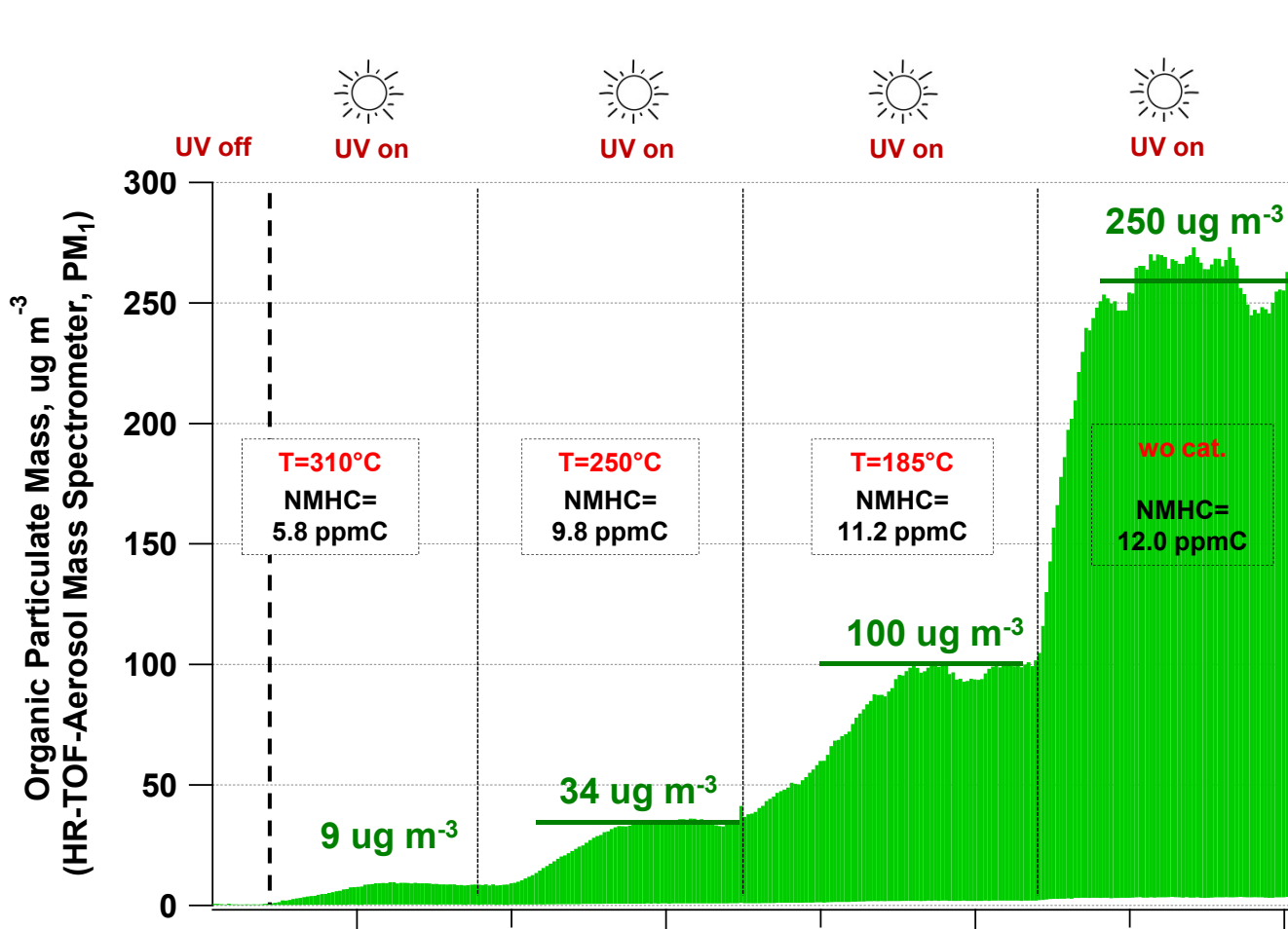
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Secondary organic aerosol formation w/wo catalyst

Cat A

Secondary Organic Particulate Mass



Estimated Reduction:

310°C

250°C

185°C

NMHC

-52%

-18%

-7%

SOA

-96%

-86%

-60%

- conversion of aromatics?
- adsorption of high molecular weight compounds to catalyst surface area?

CONCLUSIONS

- Tested catalysts work very well for CH₄ conversion in lab test and with wood burning exhaust, light off temperature should be further reduced.
- Low conversion temperatures for CO and NMHC, unclear why CeO₂ did not increase the catalyst efficiency for this conversion.
- Aromatic hydrocarbons (important SOA precursors) removed already at low catalyst temperatures (e.g. burner start up)
- SOA formation can be potentially reduced by a large proportion – requires further analysis of gasphase HC species
- *Open questions:*
 - Stability to H₂O and in long term?
 - Effect on primary PM
 - Stability > 600°C
 - Alternatives to Pt based catalysts, especially for NMHC conversion?

THANK YOU FOR YOUR ATTENTION!

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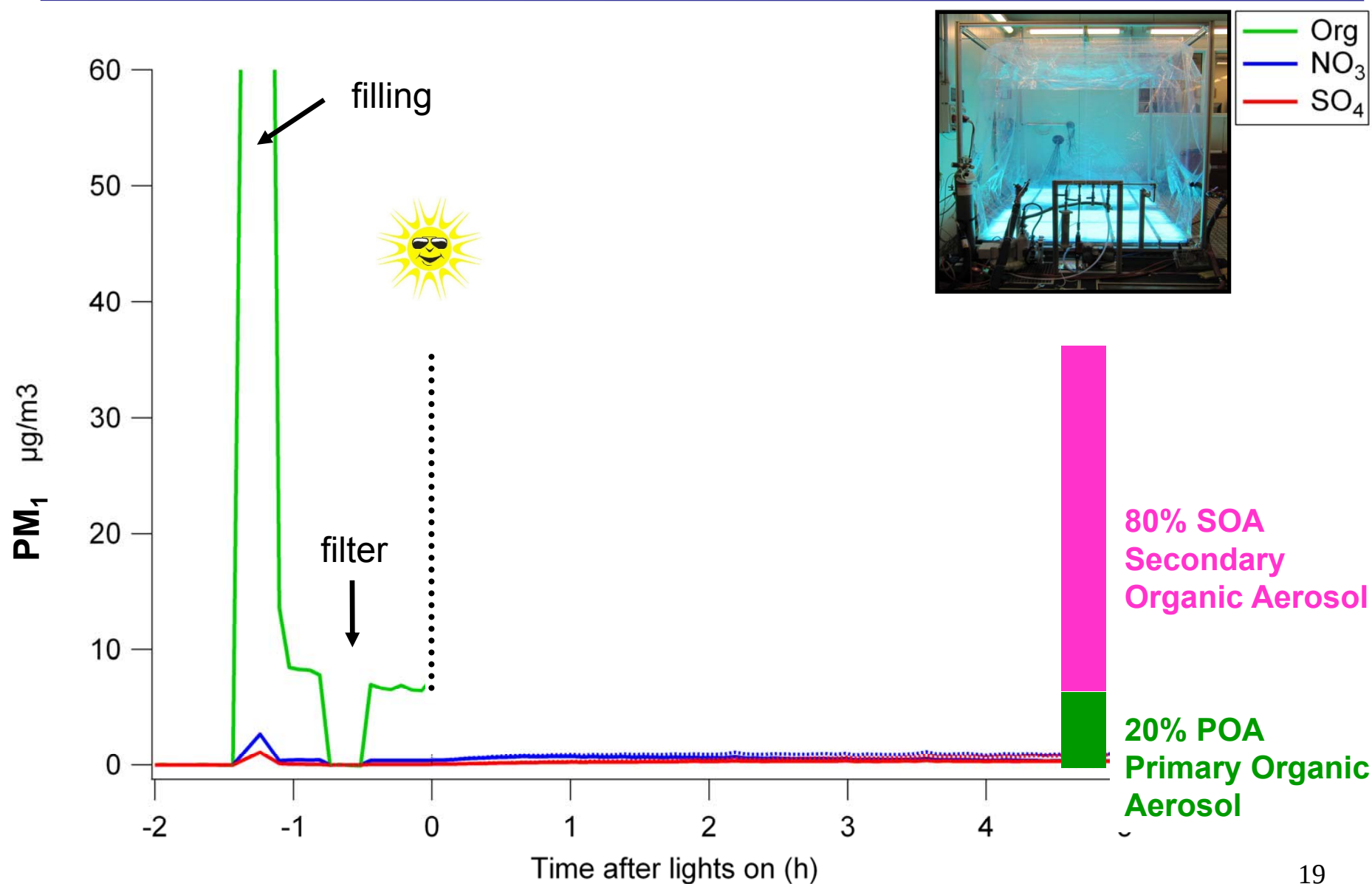
Acknowledgements

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We thank René Richter, Felix Klein and Maarten Heringa for their contribution to the work presented in this presentation.

BACK UP SLIDES

SECONDARY ORGANIC AEROSOL



(Heringa et al., 2011, SOA formation in smog chamber)

CATALYTIC SYSTEMS

Why this material?

Pt/Al₂O₃ ("Cat B") and Pt/x%CeO₂-Al₂O₃ ("Cat A")

Al₂O₃

- widely used in catalysis
- great mechanical properties
- high surface area - porosity
- water resistant

Pt

- high activity for combustion of CO and HC
- fair stability against poisoning

CeO₂

- high oxygen storage capacity (OSC)
- improves dispersion of supported metal:
smaller metal clusters,
more active centers in metal-support interface
- enhances catalysts thermal stability

(Kampolis et al., in prep.)

Preparation

Pt/Al₂O₃ ("Cat B") and Pt/x%CeO₂-Al₂O₃ ("Cat A")

Powder

Pt

- wet impregnation (WI) of H₂PtCl₆ on the commercial γ-Al₂O₃ support (200 μm), Pt content: 1.3 wt%
- drying at 90 °C overnight, calcination at 500 °C (50 °C/min) for 2h

substrate pretreatment for Pt/x%CeO₂-Al₂O₃

- deposition-precipitation (DP) of Ce(NO₃)₃·6H₂O on commercial γ-Al₂O₃, x= 10, 20, 30 wt%
- drying at 90 °C overnight, calcination at 500 °C (50 °C/min) for 2h

Monolith

- ceramic monoliths of appropriate size
- aluminum-based binder (γ-Al₂O₃, 5-10 μm)
- calcination at 500 °C in air for 2 h, hydrothermal aging at 600 °C for 6h, using 10% H₂O/N₂

POTENTIAL AEROSOL MASS (PAM)

Potential Aerosol Mass (PAM) Chamber (Kang et al., ACP, 2007 and Lambe et al, AMT, 2010)

Continuous Flow Reactor, Residence time ca 2 min,

main oxidants O_3 , OH, HO_2

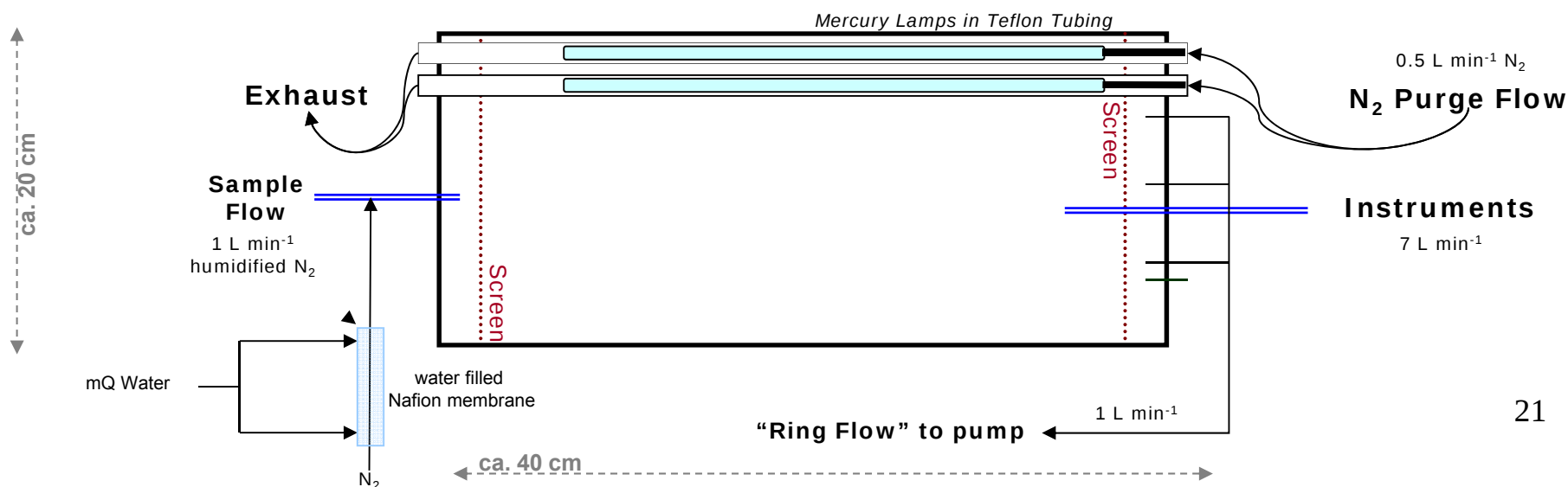
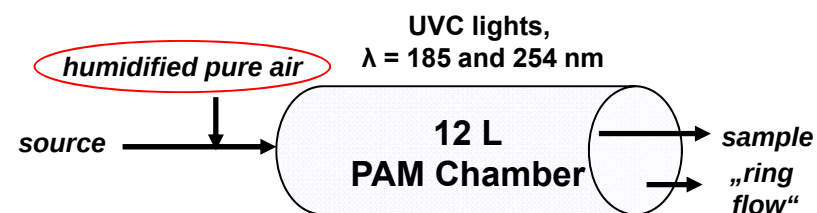
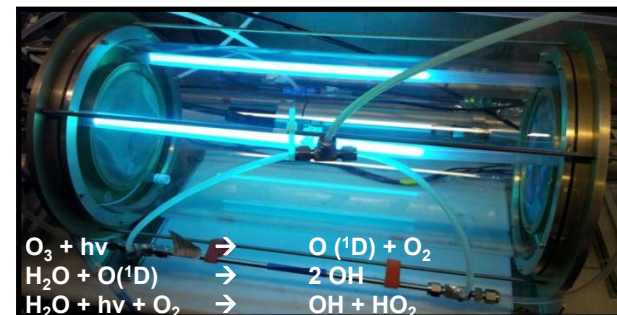
O_3 source: - photolysis of O_2

OH source: - photo-dissociation of O_3 , reaction of $O(^1D) + H_2O$;
- photolysis of H_2O

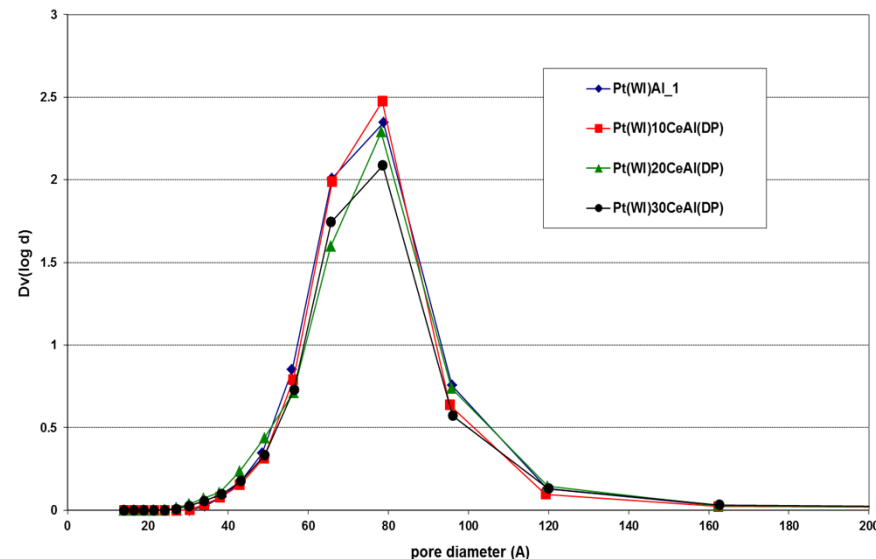
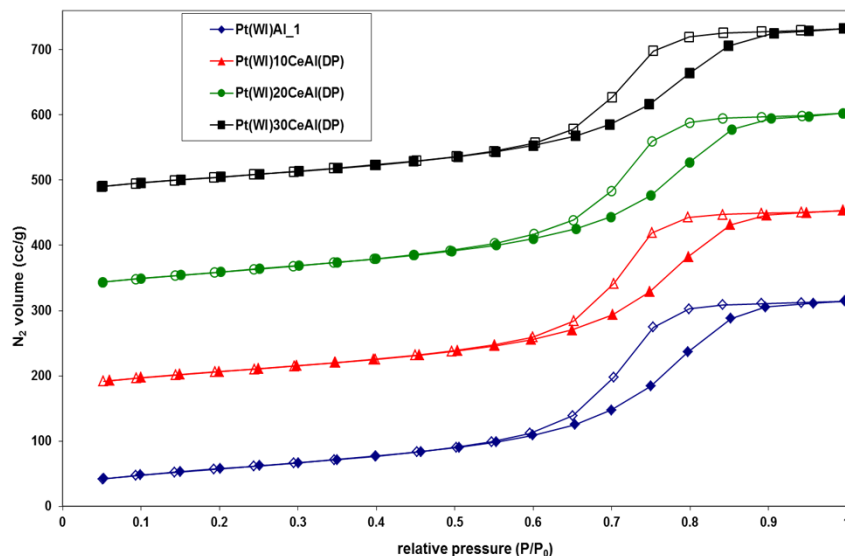
Photochemical age can be varied,

e.g. UV intensity and H_2O (g)

(OH up to 400 ppt_v ($\sim 10^{13}$ molecules / cm³), O_3 up to 15 ppm_v)



BET and Porosity of Pt/xCeO₂-Al₂O₃ catalysts



- Textural characteristics: unaffected by CeO₂
- Mesoporous structure

Catalyst	BET (m ² /g)	Pore volume (cm ³ /g)	Pore size (Å)
Pt(WI)Al	209	0.519	66.0
Pt(WI)10CeAl(DP)	205	0.499	78.6
Pt(WI)20CeAl(DP)	216	0.490	78.3
Pt(WI)30CeAl(DP)	199	0.459	78.7 ₂₂