



Effect of physical-chemical soot properties on the kinetics of catalytic soot oxidation

Steffen Wagloehner, Sven Kureti

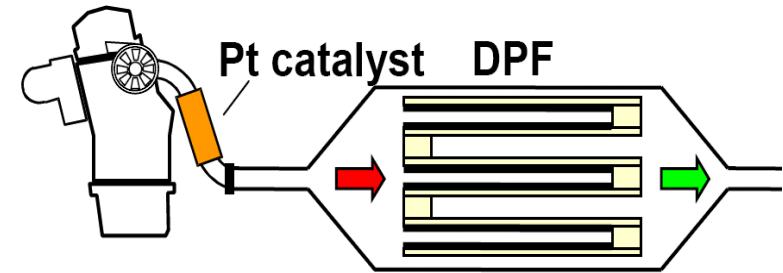
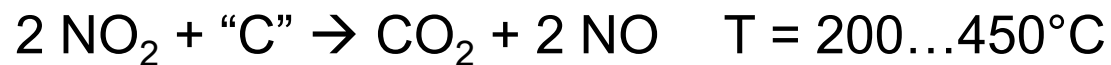
**Department of Energy Process Engineering
and Chemical Engineering**

Chair of Reaction Engineering

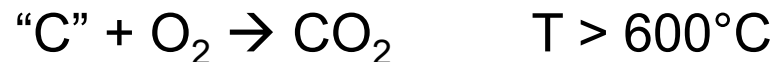


Strategies of DPF regeneration

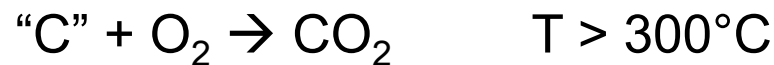
- Continuously Regenerated Trap (CRT)



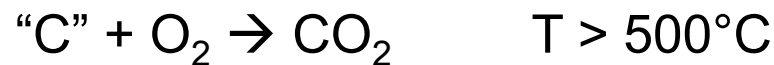
- Non-catalytic soot oxidation (induced by fuel post-injection)

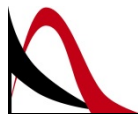


- Fuel Borne Catalyst (FBC): metal-organic compounds



- Catalytic DPF (CDPF): CeO_2 and Fe_2O_3 based catalysts





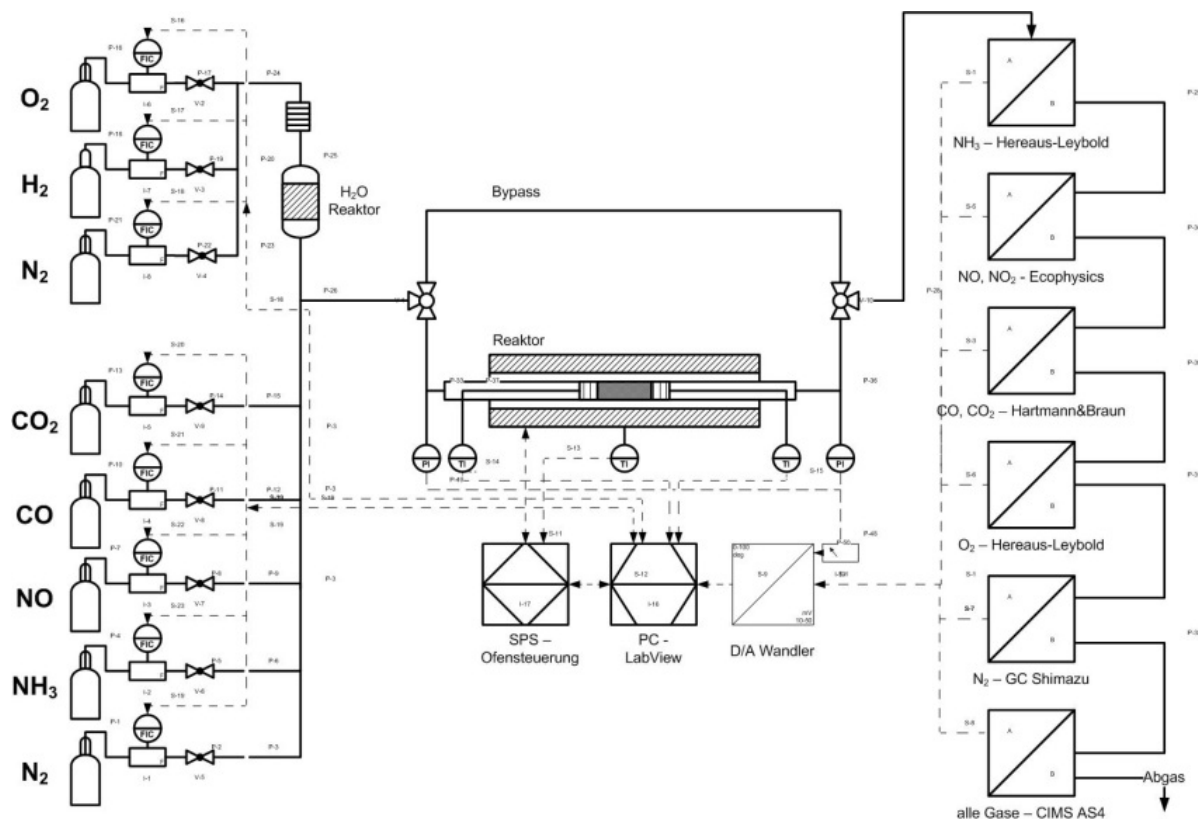
Evaluation of soot oxidation kinetics on Fe_2O_3 catalyst

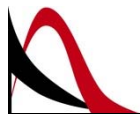
■ Temperature Programmed Oxidation (TPO)

- $n_{\text{cat}}/n_{\text{soot}} = 10 \text{ mmol} / 5 \text{ mmol}$
- $F = 500 \text{ mL/min}$, 10% O_2 , 90% N_2
- Linear heating rate: 3.3 K/min
- Mixing catalyst and soot by ball milling

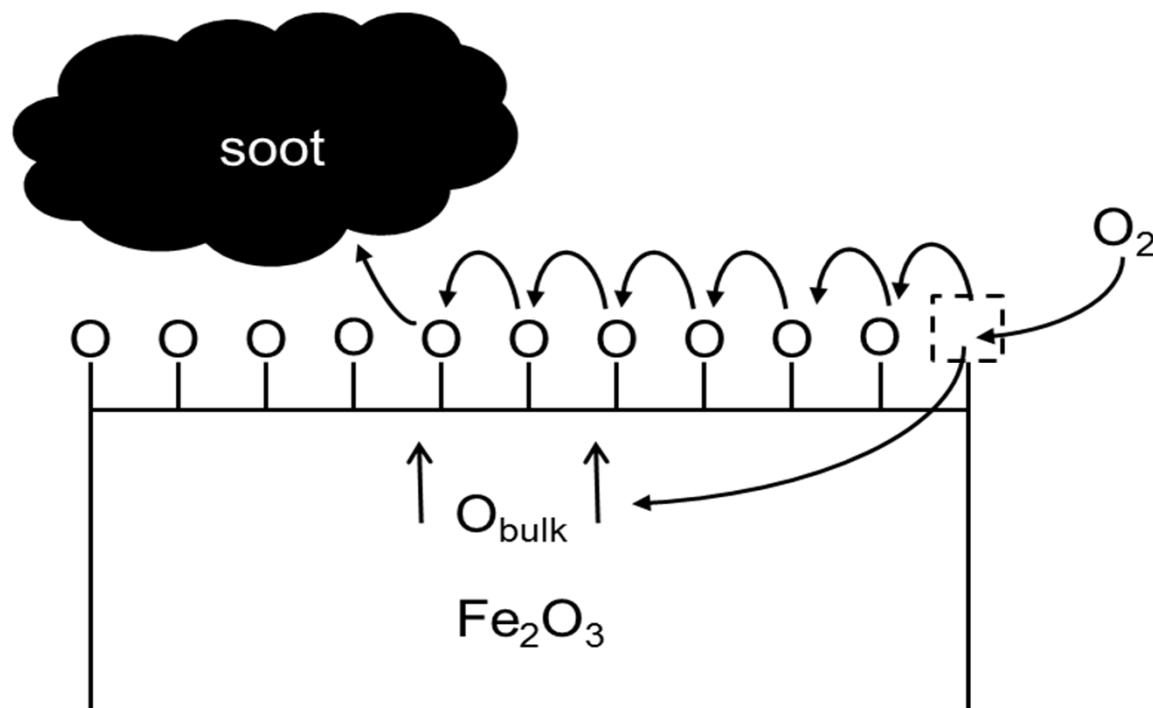


Plug flow reactor with packed bed

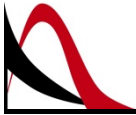




Mechanistic scheme of soot oxidation on Fe_2O_3

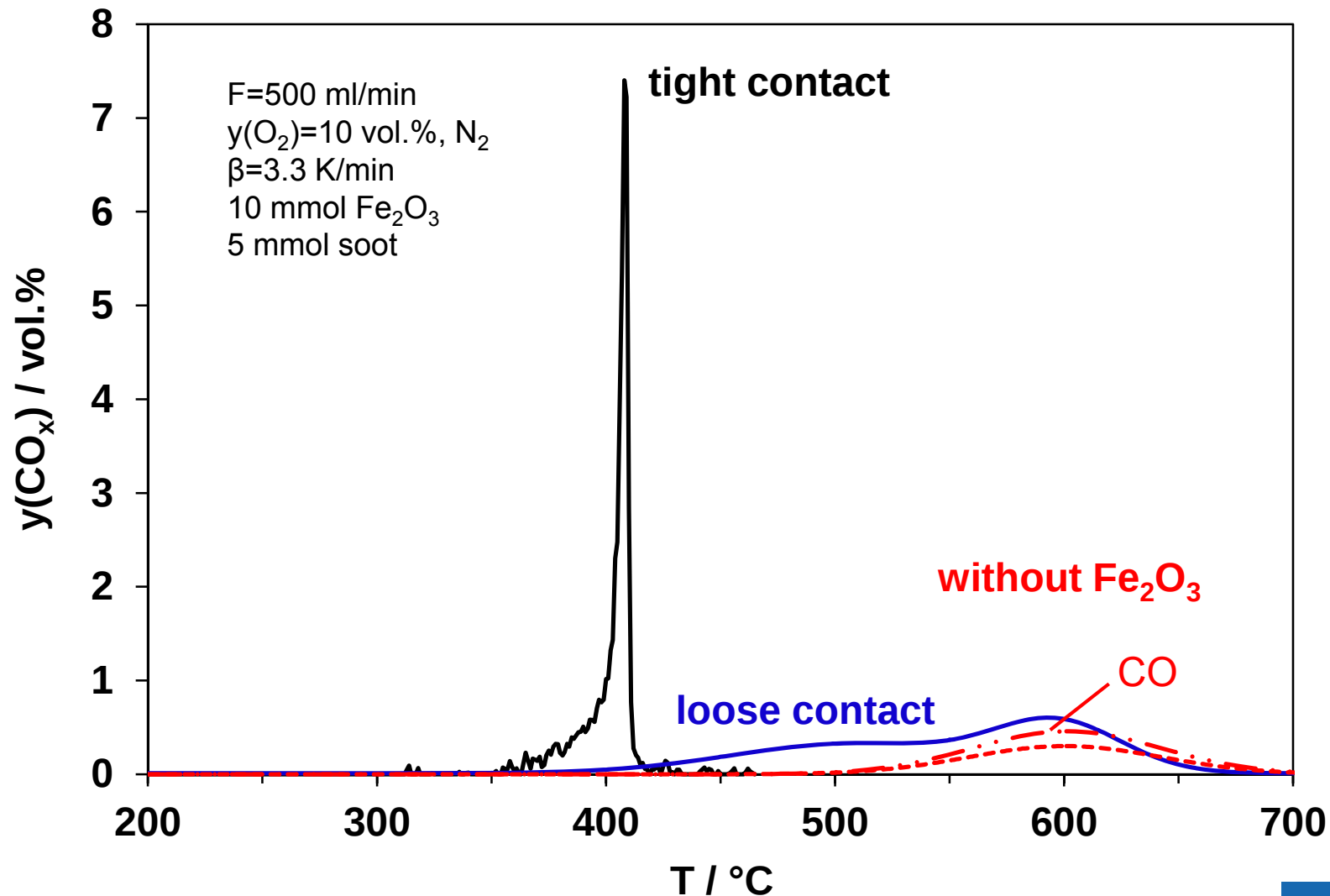


S. Wagloehner, S.Kureti, Appl. Catal. B 125 (2012) 185

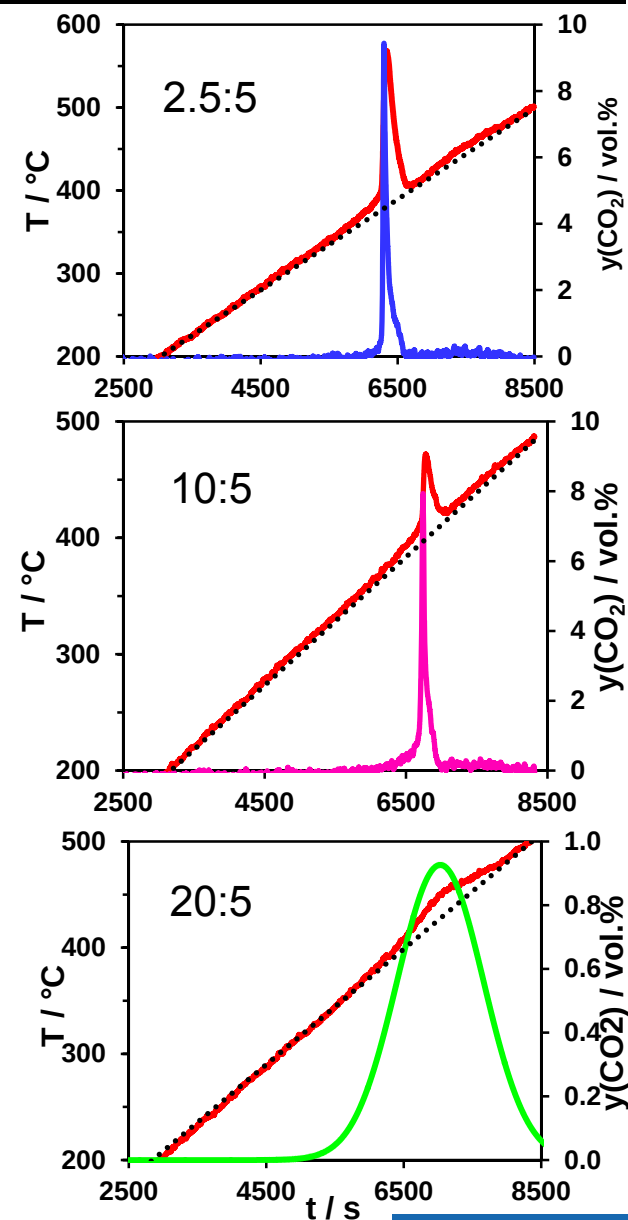
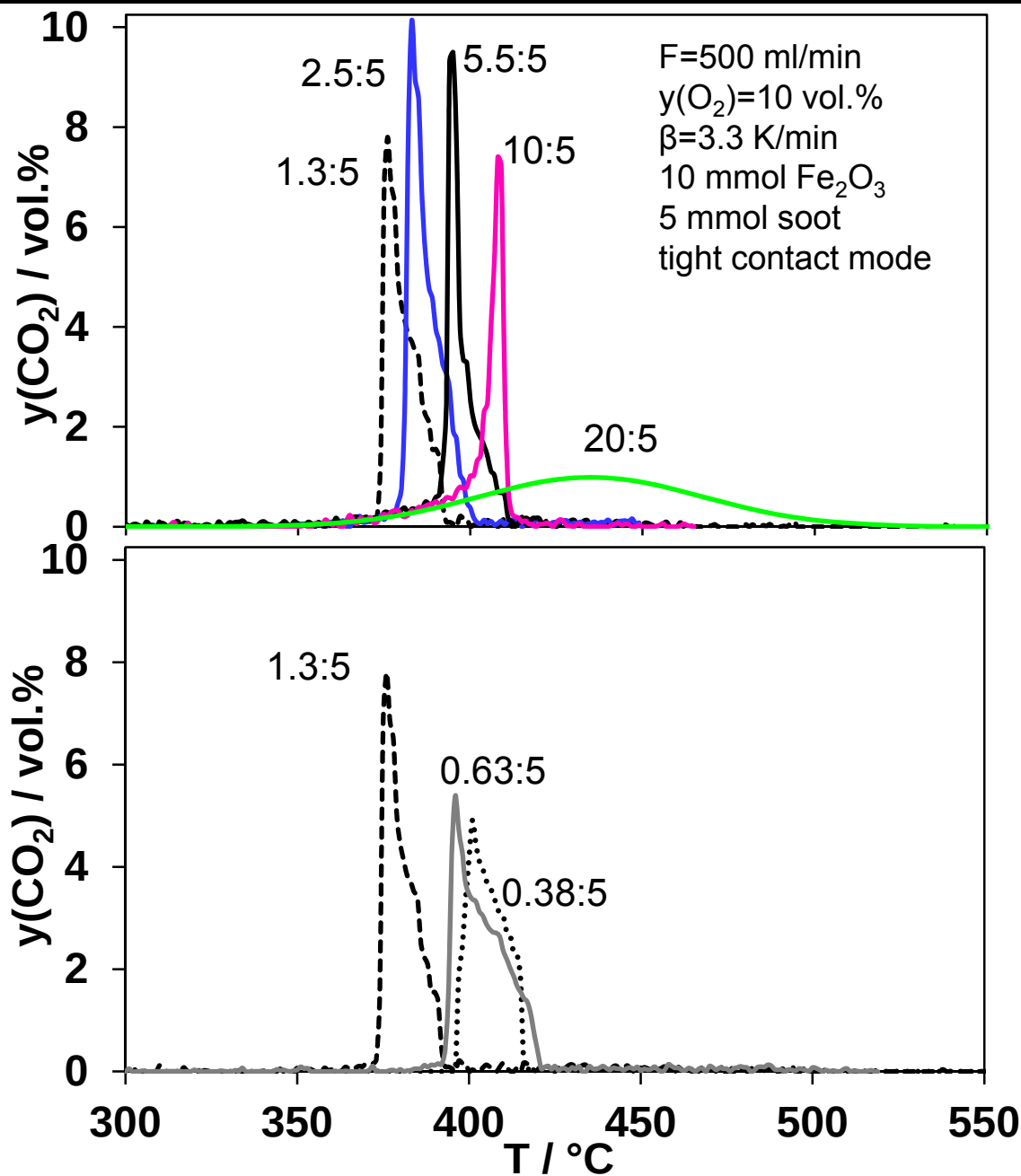


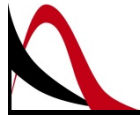
Effect of contact on soot oxidation kinetics

- Performance in tight and loose contact vs. bare soot



Effect of catalyst/soot ratio on soot oxidation kinetics

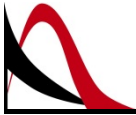




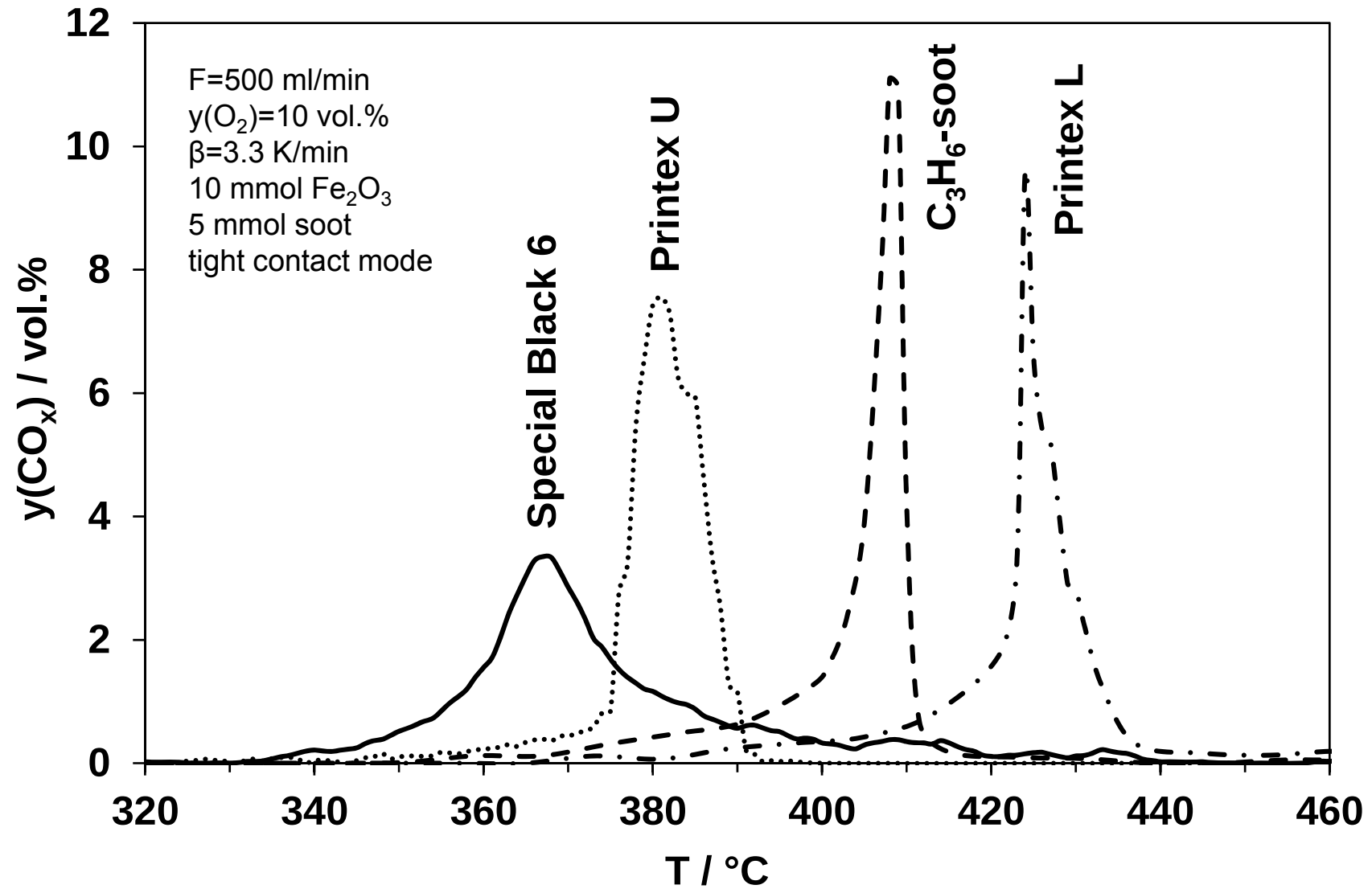
Effect of type of soot on catalytic oxidation kinetics

- 4 different types of model soot
 - C_3H_6 -soot (home-made)
 - Printex U
 - Special Black 6
 - Printex L
- soot formed at full load
- soot formed at partial load
- mature soot
- Detailed physical-chemical analysis of the model soot samples (ashless)

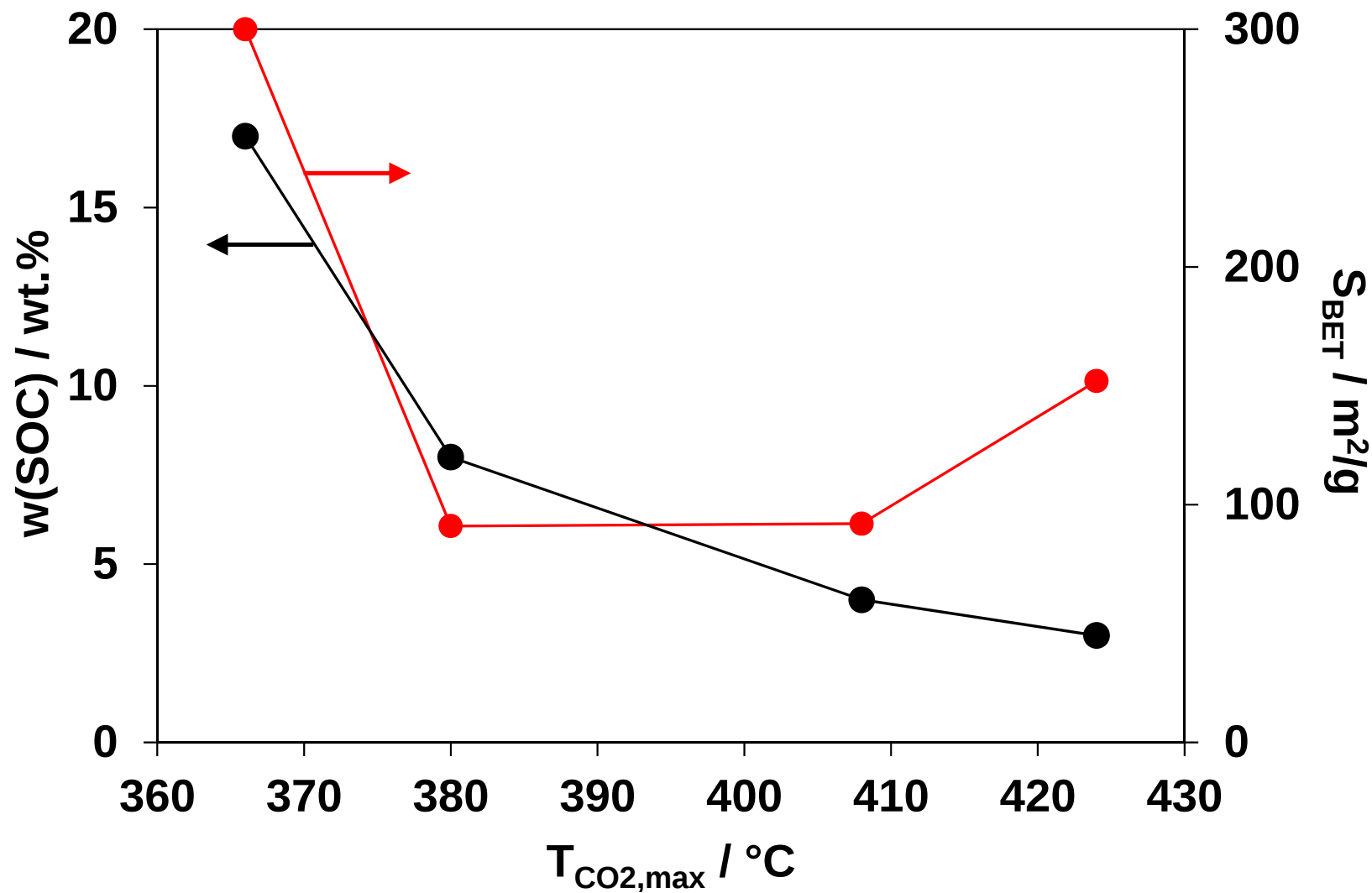
	Ultimate analysis				Proximate analysis					
	C	H	N	O	HHV	S_{BET}	W_{H_2O}	VM	W_{CO}	W_{CO_2}
	[wt.%]				[MJ/kg]	[m ² /g]		[wt.%]		
Special Black 6	89.5	0.4	0.6	9.0	29.86	300	5	17	8.0	15.2
Printex U	96.7	0.7	0.3	2.0	33.37	91	2	8	3.1	5.6
C_3H_6 -Soot	97.5	0.6	0.2	1.5	33.35	92	0	4	2.8	4.1
Printex L	99.2	0.1	0.3	0	33.47	152	1	3	0.5	2.5

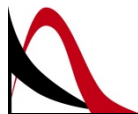


Effect of type of soot on catalytic oxidation kinetics

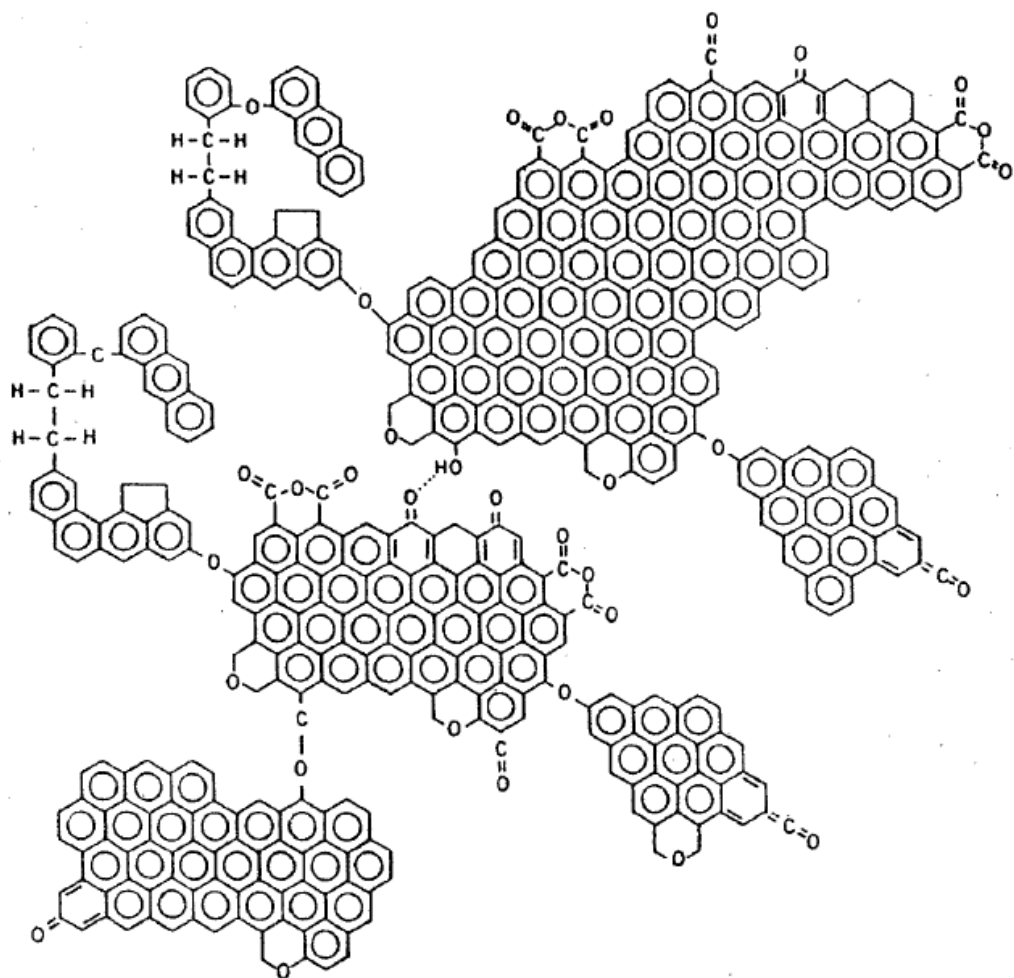


Correlation of catalytic oxidation kinetics with soot properties

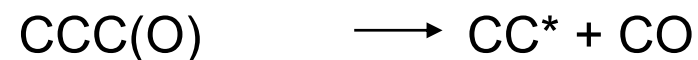
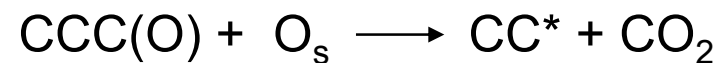




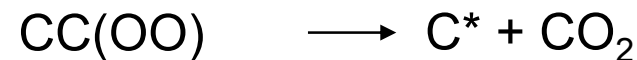
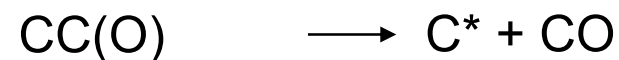
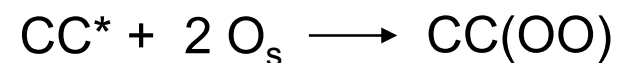
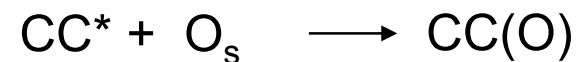
Role of surface oxygen compounds (SOC) of soot



Reactions of SOC:

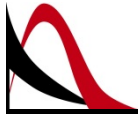


Subsequent reactions on soot:



M.S. Akhter et al.,
Appl. Spectrosc. 39 (1985) 143

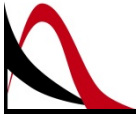




Summary

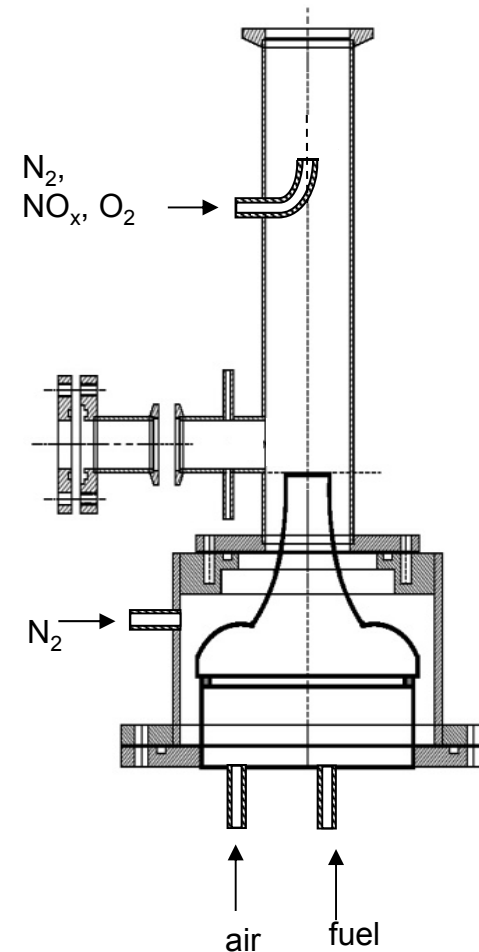
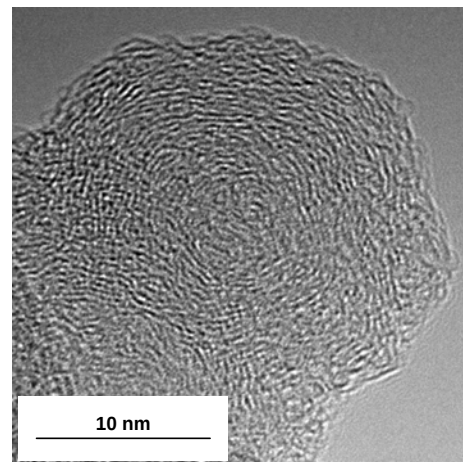
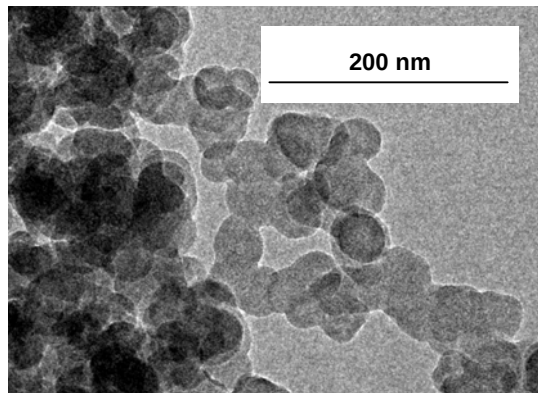
- Fe_2O_3 is an effective catalyst for soot oxidation
- Soot oxidation kinetics depend on type of contact, local heat evolution and type of soot
- SOC determine the kinetics of soot oxidation on Fe_2O_3 catalyst
- SOC are the initial precursors of carbon sites supplied by oxygen from the Fe_2O_3 catalyst

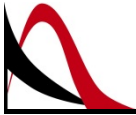
We thankfully acknowledge the financial support from Umicore.



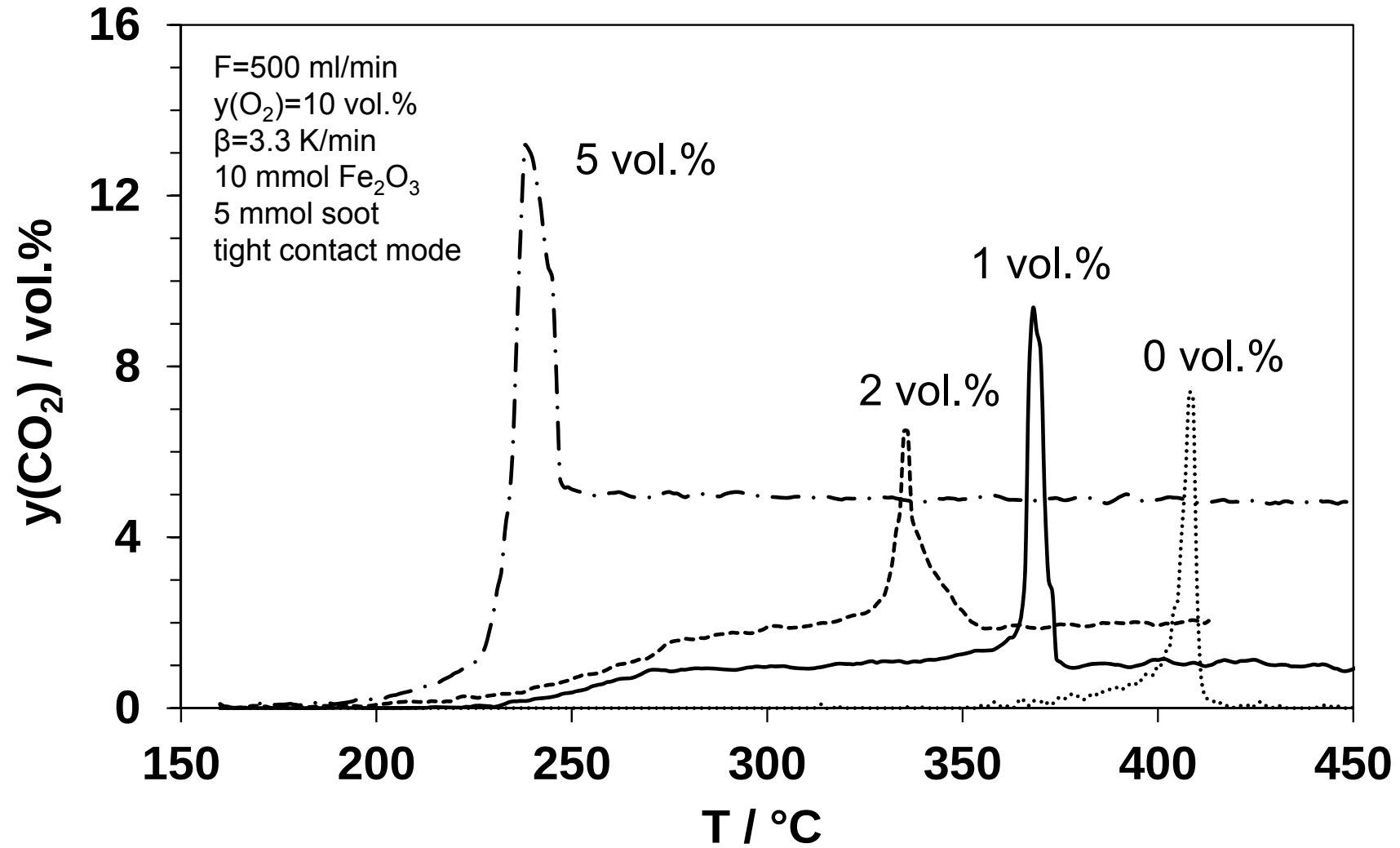
Production of realistic diesel model soot

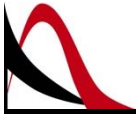
- Diffusion burner ($\text{C}_3\text{H}_6/\text{O}_2$ flame)
- Physical-chemical properties
 - 2.6 wt.% adsorbed
 - 98.8 wt.% C
 - 0.7 wt.% O
 - 0.5 wt.% H
 - Most frequent diameter: ca. 45 nm
 - $S_{\text{BET}} = 90 \text{ m}^2/\text{g}$





Effect of CO on soot oxidation kinetics on Fe_2O_3

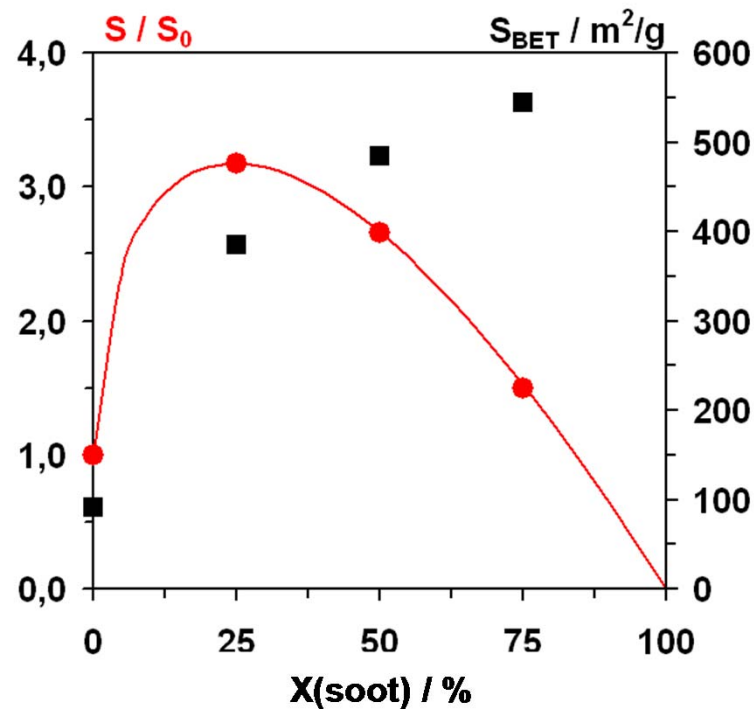




Global kinetic model

$$r(\text{CO}_x) = k_{\text{CO}_x} \cdot n(\text{C}_f) \cdot c(\text{O}_2)$$

$$k_{\text{CO}_x} = A_{\text{CO}_x} \exp(-E_{\text{CO}_x}/RT)$$



From TPD with $X(\text{C}) = 0, 25, 50, 75\%$:

$$\rightarrow \frac{n(\text{CO}_x)_{\text{des}}}{S(X)} = 8,7 \frac{\mu\text{mol}}{\text{m}^2} = \lambda$$

From evolution of S_{BET} :

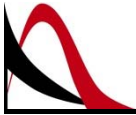
$$\rightarrow S(X) = S_0 \cdot m_0 \cdot (1-X) \cdot (1+60 \cdot X)^{1/2}$$

$$\rightarrow n(\text{C}_f) = \lambda \cdot S(X)$$

S.K. Bhatia, D.D. Perlmutter,
J. Am. Inst. Chem. Eng. 26 (1980) 379

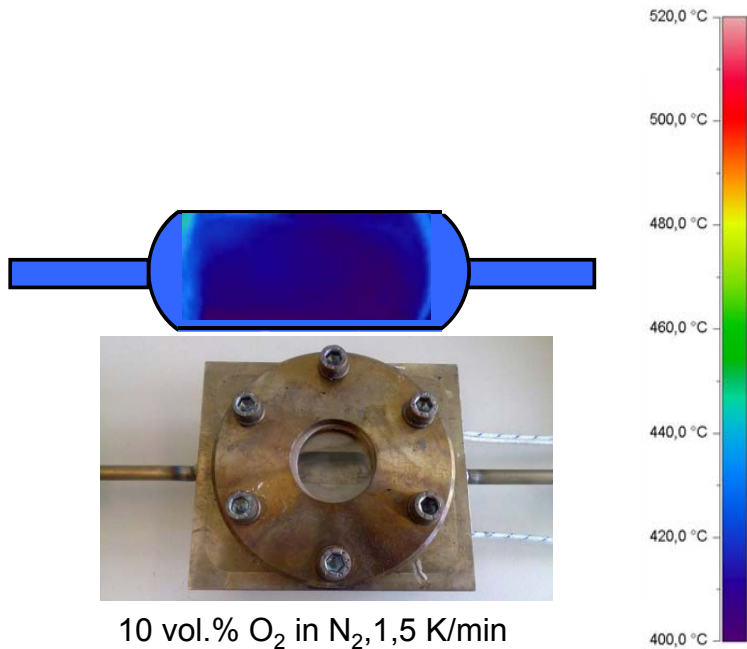
$$\rightarrow r(\text{CO}_x) = A_{\text{CO}_x} \cdot \exp(-E_{\text{CO}_x}/RT) \cdot S_0 \cdot m_0 \cdot (1-X) \cdot (1+60 \cdot X)^{1/2} \cdot \lambda \cdot c(\text{O}_2)$$





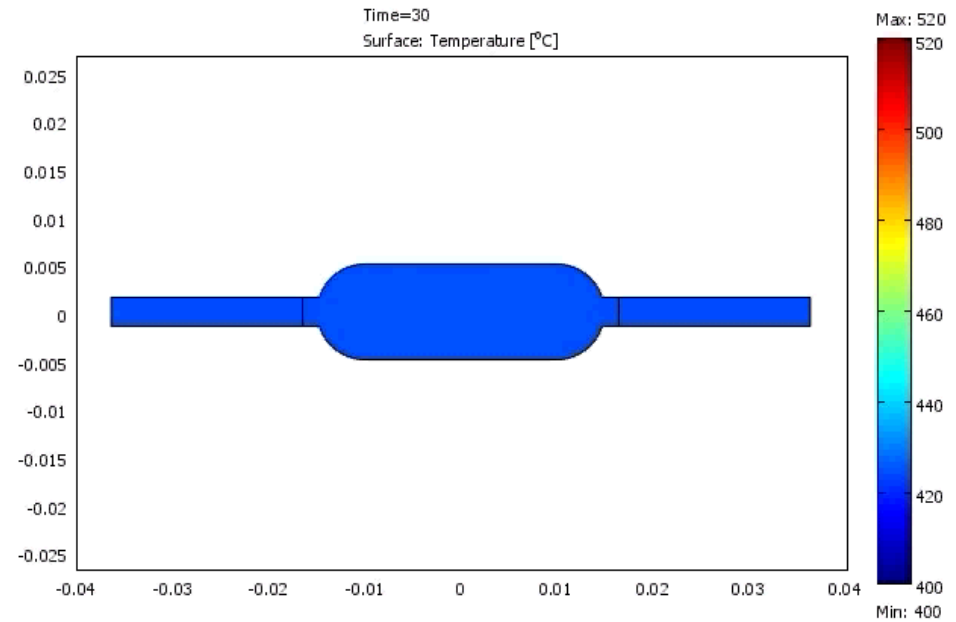
Experiment vs. Simulation

Experiment

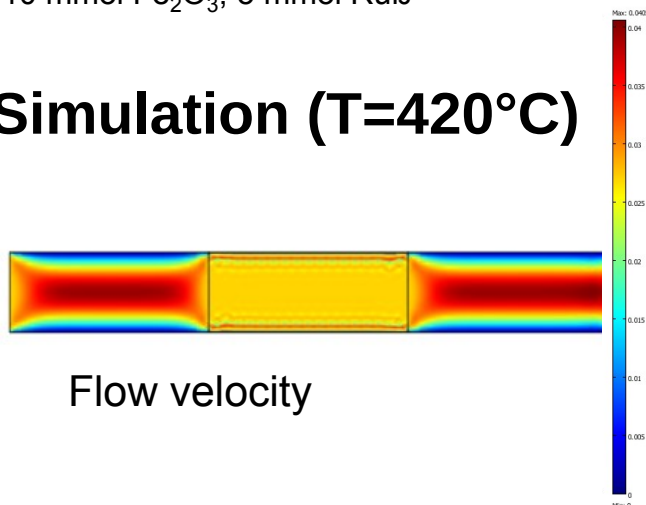


10 vol.% O₂ in N₂, 1,5 K/min
10 mmol Fe₂O₃, 5 mmol Ruß

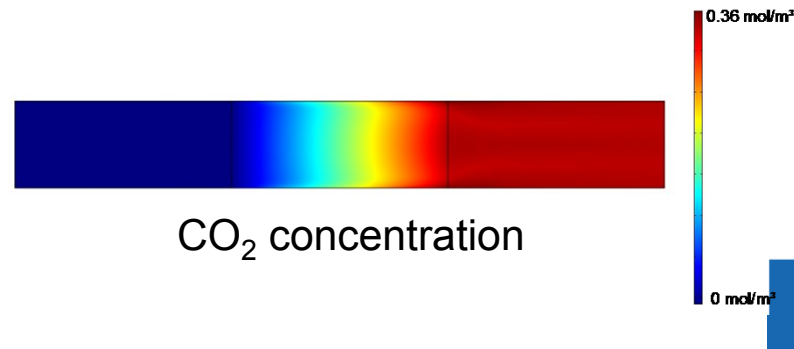
Simulation



Simulation (T=420°C)



Flow velocity



CO₂ concentration