

# Mechanism of the catalytic soot oxidation on $\text{Fe}_2\text{O}_3$

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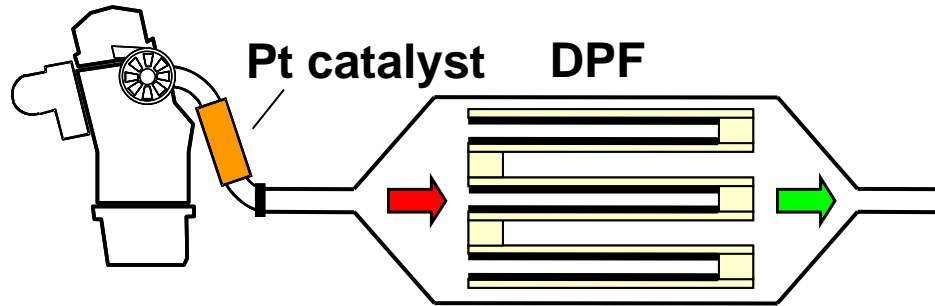
# Content

- **Introduction**
- **Experimental studies**
- **Mechanistic model for the soot oxidation on  $\text{Fe}_2\text{O}_3$  catalyst**
- **Outlook**



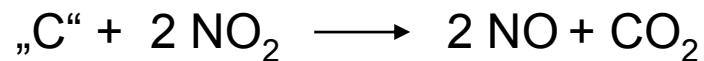
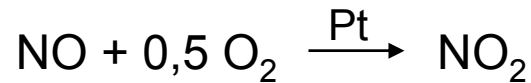
# Removal of soot from diesel exhaust

- Separation of soot by Diesel Particulate Filters (DPF)



- DPF regeneration

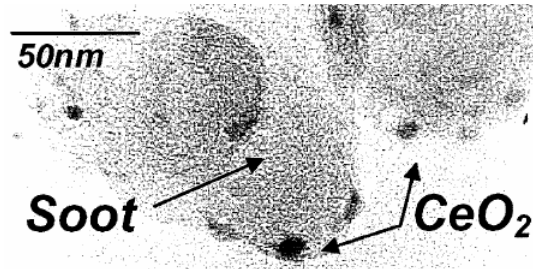
- Continuously Regeneration Trap (CRT)



- Catalytic DPF (C-DPF)



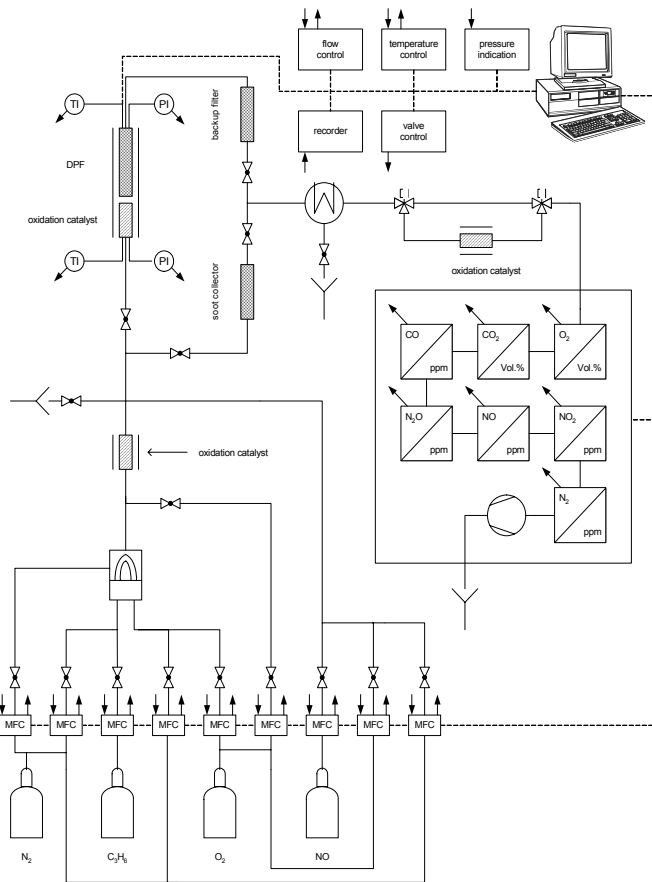
- $\text{CeO}_2$  and  $\text{Fe}_2\text{O}_3$  originated from Fuel Borne Catalysts (FBC) enhance oxidation of deposited soot



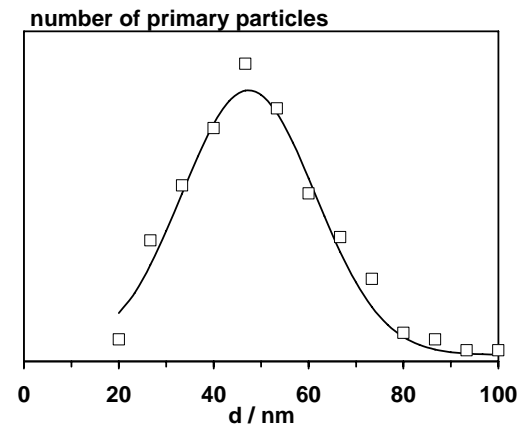
K. Ohno, Ph.D. thesis, 2006

**→  $\text{Fe}_2\text{O}_3$  reveals practical relevance for catalytic soot oxidation**

- In our mechanistic studies:  $\alpha$ -Fe<sub>2</sub>O<sub>3</sub> and a C<sub>3</sub>H<sub>6</sub> soot are used
- Model soot prepared by diffusion burner (C<sub>3</sub>H<sub>6</sub>/O<sub>2</sub> flame)



- 2.6 wt.% adsorbed species
- 98.8 wt.% C  
0.7 wt.% O  
0.5 wt.% H  
0 wt.% N
- $S_{\text{BET}} = 65 \text{ m}^2/\text{g}$
- $d = 45 \text{ nm}$  (most frequent diameter)



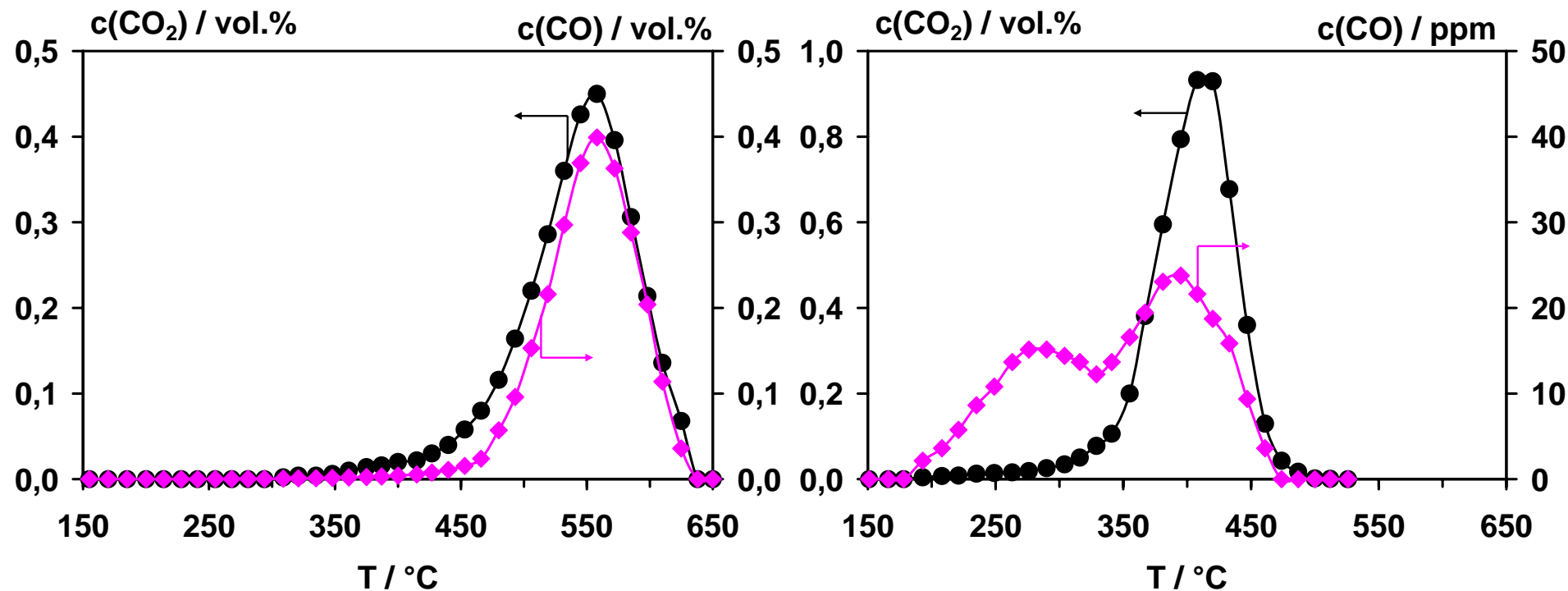
P. Balle, H. Bockhorn, B. Geiger, N. Jan, S. Kureti, D. Reichert, T. Schröder, *Chem. Eng. Process.* 45 (2006) 1065



# Effect of the $\text{Fe}_2\text{O}_3$ catalyst in Temperature Programmed Oxidation (TPO) of the soot

without catalyst

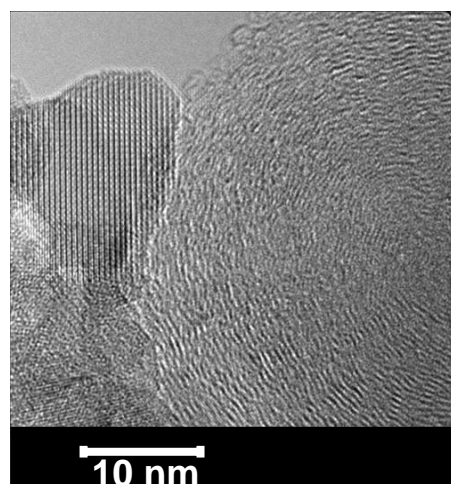
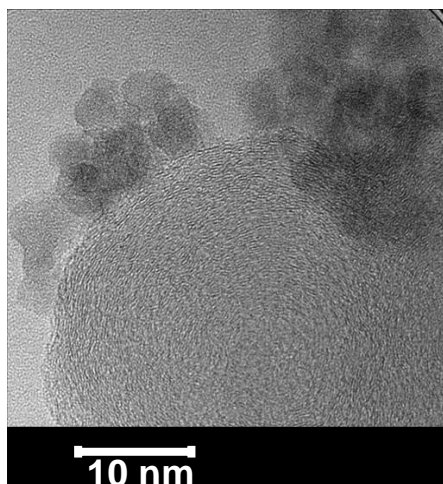
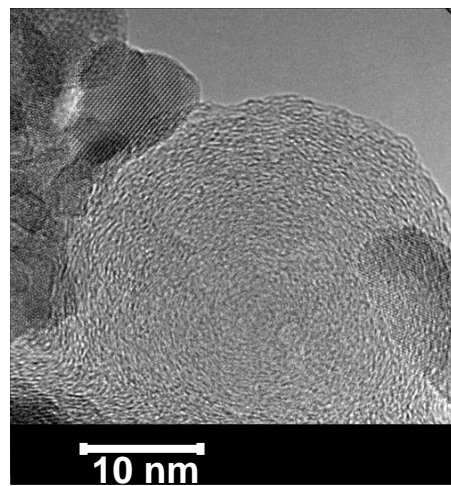
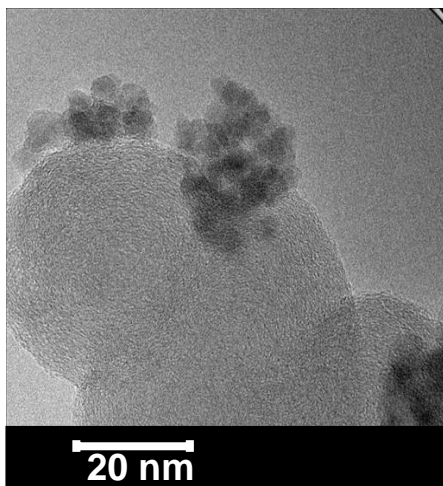
with  $\text{Fe}_2\text{O}_3$  catalyst



Conditions:  $c(\text{O}_2)=6.0 \text{ vol.}\%$  Flow: 500 ml/min (STP)  $\Delta T/\Delta t=90 \text{ K/h}$   
 $c(\text{N}_2)=94 \text{ vol.}\%$   $n(\text{Fe}_2\text{O}_3)=20 \text{ mmol}$   $n(\text{C})=10 \text{ mmol}$



# Development of the contact between $\text{Fe}_2\text{O}_3$ catalyst and soot (HRTEM study)



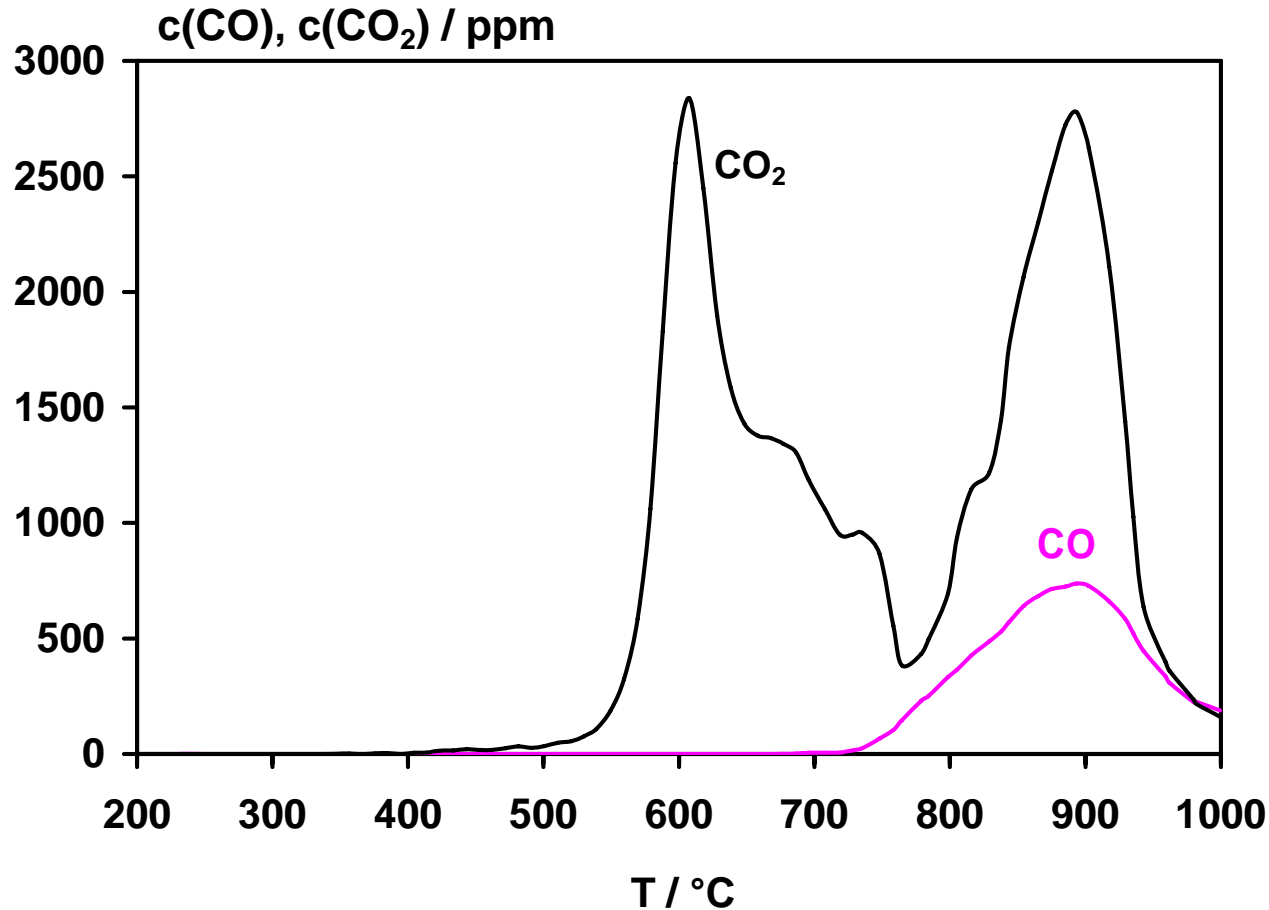
**X(soot) = 0%**

**X(soot) = 90%**

H. Bockhorn, S. Kureti,  
D. Reichert, *Top. Catal.* (2007)



# Carbothermal reaction



Conditions:

$c(\text{O}_2) = 0 \text{ vol.}\%$

$\text{N}_2$  balance

$n(\text{Fe}_2\text{O}_3) = 20 \text{ mmol}$

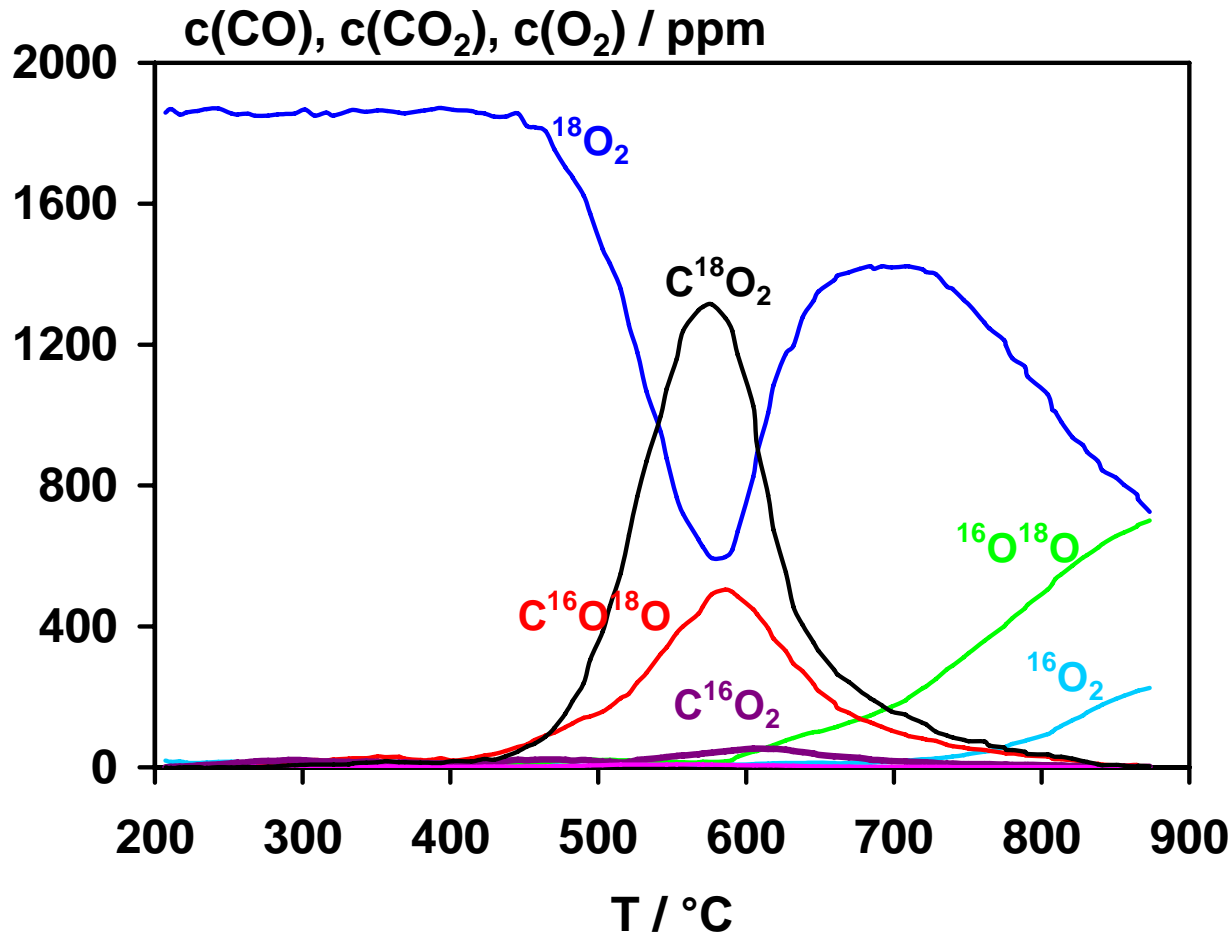
$n(\text{C}) = 10 \text{ mmol}$

$\Delta T / \Delta t = 90 \text{ K/h}$





# TPO with isotope labelled oxygen ( $^{18}\text{O}_2$ )



Conditions:

$c(\text{O}_2)=0.19 \text{ vol.}\%$

$\text{N}_2$  balance

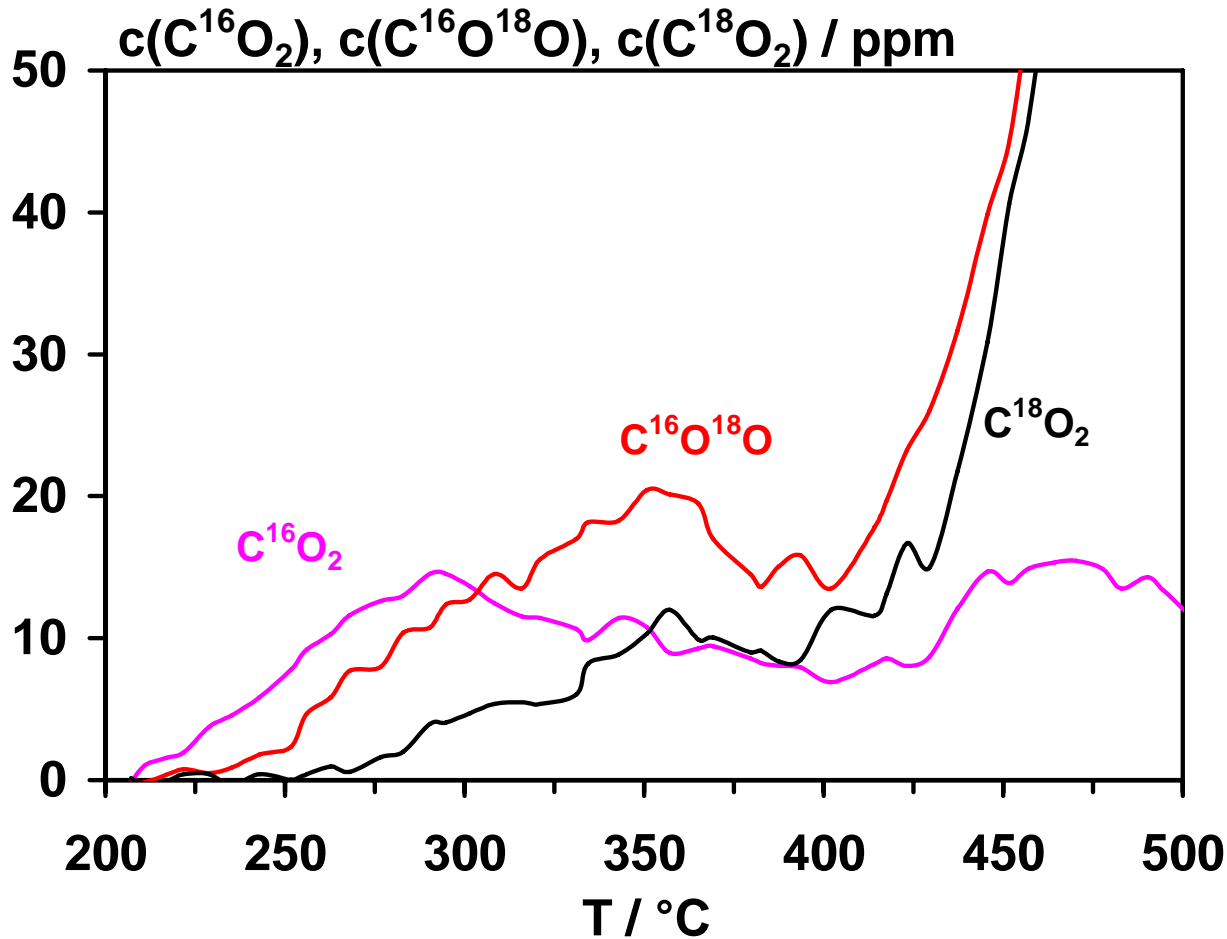
$n(\text{Fe}_2\text{O}_3)=3.8 \text{ mmol}$

$n(\text{C})=1.9 \text{ mmol}$

$\Delta T/\Delta t=600 \text{ K/h}$



# Starting period of the isotopic TPO



Conditions:

$c(\text{O}_2)=0.19 \text{ vol.}\%$

$\text{N}_2$  balance

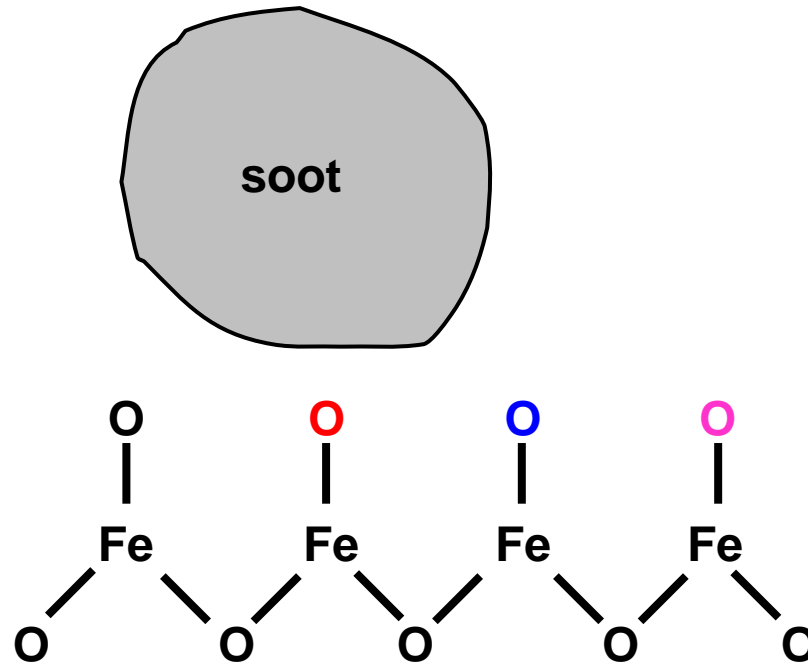
$n(\text{Fe}_2\text{O}_3)=3.8 \text{ mmol}$

$n(\text{C})=1.9 \text{ mmol}$

$\Delta T/\Delta t=600 \text{ K/h}$



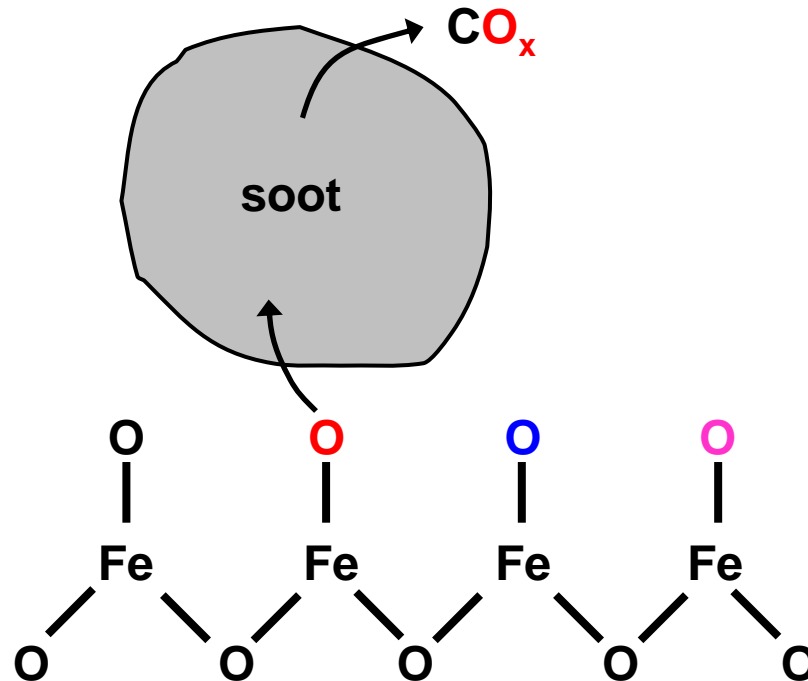
# Model for the effect of $\text{Fe}_2\text{O}_3$ catalyst on soot oxidation



H. Bockhorn, S. Kureti, D. Reichert, *submitted*



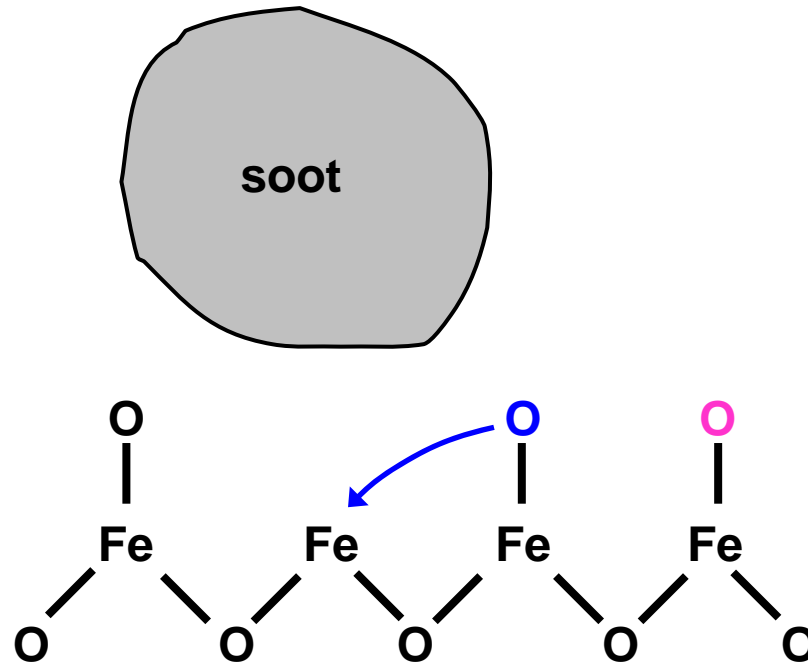
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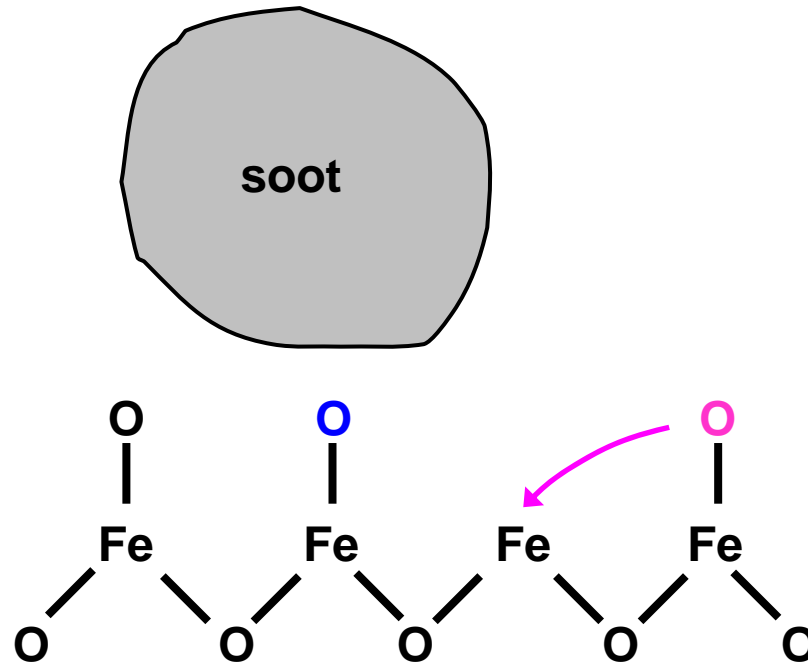
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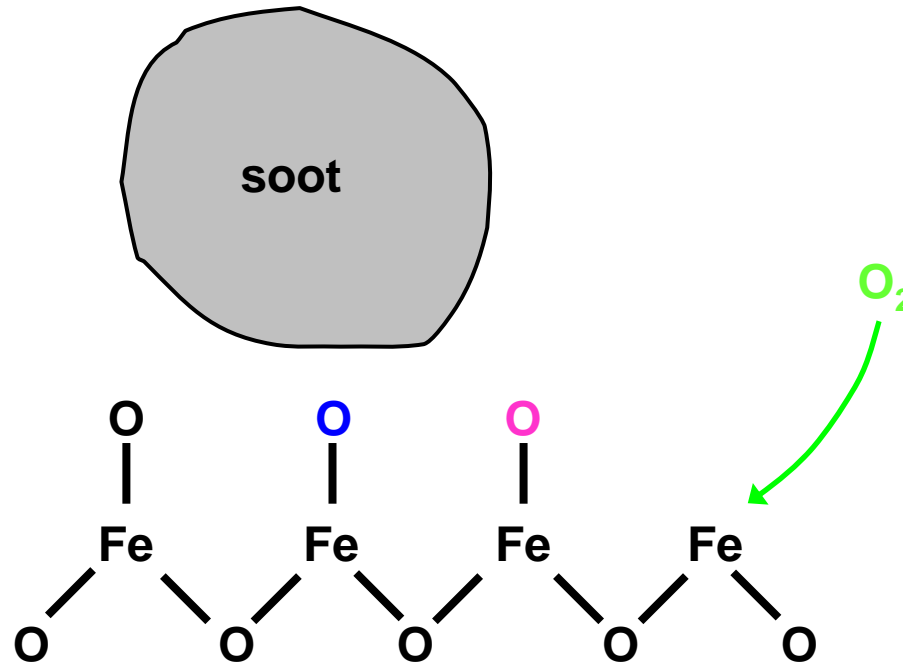
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# Summary

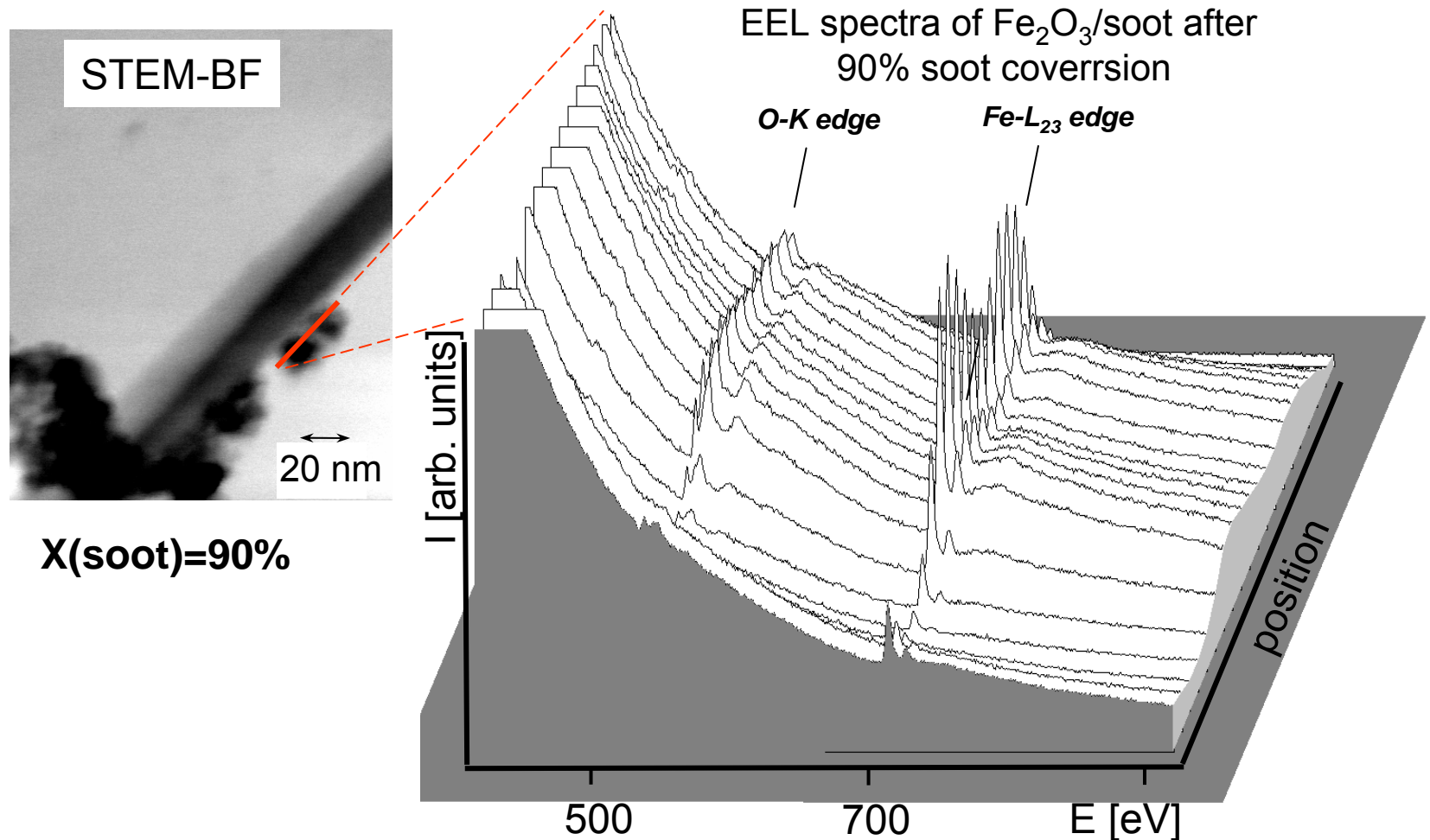
- **Fe<sub>2</sub>O<sub>3</sub> catalyst enhances the soot oxidation**
- **Fe<sub>2</sub>O<sub>3</sub> catalyst transfers the gas-phase oxygen to the soot at the contact points**
- **Gas-phase oxygen adsorbs dissociatively on O vacancies and migrates on the Fe<sub>2</sub>O<sub>3</sub> surface to the contact points**
- **Contact between catalyst and soot maintains up to high conversion levels**
- **Catalyst is not directly involved in the soot/oxygen reaction**





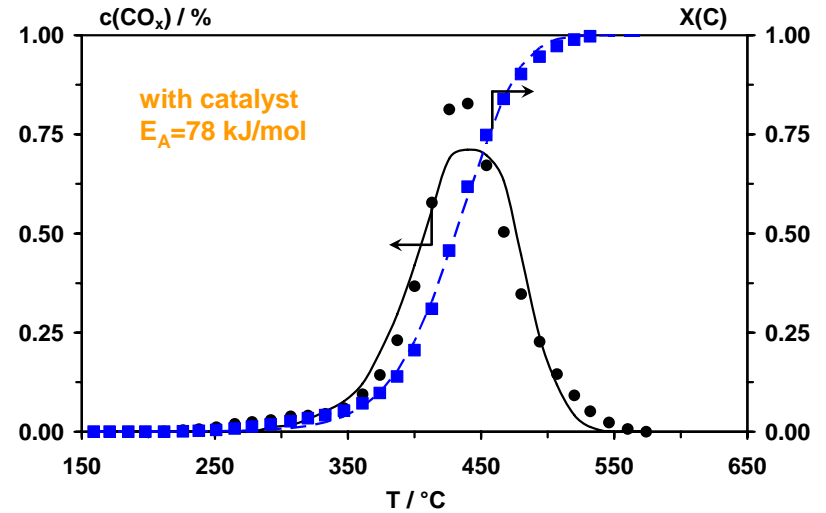
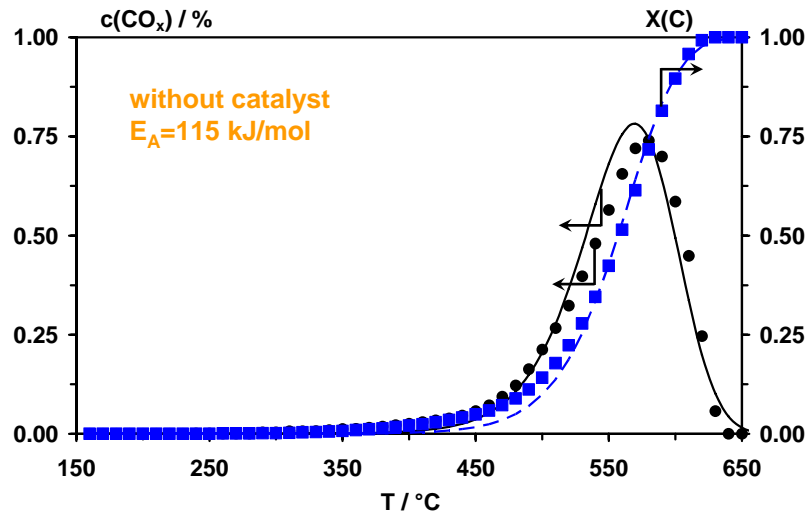
# Outlook and current activities

- Study of the interaction between soot and  $\text{Fe}_2\text{O}_3$  in the sub-nm range



- Kinetic modelling

$$\beta \cdot \frac{dX}{dT} = A \cdot e^{\left(\frac{E_A}{RT}\right)} \cdot \lambda \cdot S_0 \cdot m_0 \cdot (1-X) \cdot \sqrt[3]{1+f \cdot X \cdot c(O_2)^{n_{O_2}}}$$



- Development of improved  $Fe_2O_3$  catalysts

